# EXPERIMENTAL INVESTIGATION ON THE PERFORMANCE OF COMPRESSED AIR ENERGY STORAGE USING SPRAY-BASED HEAT TRANSFER

by

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Near-isothermal compression and expansion may be accomplished by injecting water droplets into the air during the process to increase the overall efficiency. However, little is known about the relationship between spray system parameters and compressed air energy storage (CAES). Furthermore, the experiments about CAES using spray-based heat transfer have not been investigated. The aim of this paper is to study the relationship between the performance of CAES and the spray system parameters by experimentally. The parameters including the spray closing time, the spray opening time, and the nozzle diameter are discussed. Results show that under the same operating conditions, the maximum air pressure in compression chamber reach to constant value when the spray closing time is 0.6 seconds, and spraying water mist within 0.6-1.2 seconds has no heat exchange effect on the air in the cylinder. During the compression process, the smaller the nozzle diameter is, the higher maximum pressure in compression chamber is. During the expansion process, if we ignore the energy consumption of spray system, the larger the nozzle diameter is, the more the expansion output is. Further investigation is recommended to optimize spray parameters based on different CAES systems. Key words: CAES system, spray-based heat transfer, the spray closing time,

the spray opening time, the nozzle diameter

# Introduction

According to the 14<sup>th</sup> five-year plan for national economic and social development and the long-range goals for the 2030's and the 75<sup>th</sup> session of the United Nations General Assembly agreement, China has a target to carbon peak by 2030 and to carbon neutral by 2060. The government is strongly supporting renewable energy incentive policies. The newly installed wind power capacity and solar power capacity have rapidly grown since 2012. In 2022, China's newly installed wind and solar PV power generation capacity exceeded 12 GW, accounting for 60% of the newly installed power generation capacity [1]. Because of the inherent intermittency of renewable energy, power generation in renewable energy plants fluctuates over many time scales, from seconds to days which restricts direct wind power penetration into power systems. To mitigate the problem, energy storage technologies are focused on. The

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CAES technology has the advantages of large scale, environmental friendliness, long service life, and large energy storage capacity, and has broad application prospects [2].

Conventional CAES systems that burn fossil fuel have been put into commercial operation in Germany (Huntorf CAES power station which was built 1978) and USA (McIntosh CAES power station which was built in 1991) [3, 4]. The heat is recovered in compression process and reused to preheat the compressed air during expansion process in McIntosh CAES power station. So compared with Huntorf CAES power station, the plant efficiency increases 12% [5]. Currently, no fossil burning CAES systems have been proposed and applied to achieve zero carbon emission. The salt cavern CAES national pilot demonstration project in Jintan, Jiangsu Province, China, is based on the advance adiabatic CAES (AA-CAES) system. The AA-CAES system can recover and stored heat which is generated during the compression process using heat exchangers. Then, the heat is used to heat the high pressure air during expansion. The total system efficiency of 55%-61% [6]. However, most large scale CAES requires suitable geography which becomes the limiting factors, and lower efficiency affects its profitability. High pressure CAES has a high energy density and decreases the volume of compressed air which allows CAES to be free from geographical constraints [7]. Vessels with storage pressures of up to 75 MPa are already in use, and hydrogen can be stored at pressures of up to 100 MPa in hydrogen refueling stations. The work done to compress air to a pressure-ratio, r, and discharge it into a high pressure store depends on whether the air is kept cool during compression. To compress 1  $m^3/s$  of ambient air to 75 MPa, the mechanical power to the compressor is equal to 1996 kW based on adiabatic condition. But under the isothermal condition, the required mechanical power is reduced to 670.8 kW. The expander output power will increased by increasing air temperature during expansion process. So isothermal compression and expansion are an efficient method to improve CAES system efficiency due to the minimum work input and the maximum work output associated with the isothermal process.

Clearly, heat transfer plays an important role in achieving near-isothermal compression and expansion. For the isothermal compression, the instantaneous rates of heat transfer should be equal to the instantaneous mechanical power to the compressor [8]. For the isothermal expansion, the instantaneous rates of heat transfer should be equal to the expander instantaneous mechanical power output. In general, the mechanical power to the compressor and the expander instantaneous mechanical power output are significantly higher than the instantaneous rate of heat transfer. This results in a near-adiabatic process in the compressors and expanders. So convective heat transfer coefficient and area of heat transfer should be increased drastically to achieve the near-isothermal compression and expansion. Various methods for enhancing heat transfer have been investigated. Liquid piston, spray, aqueous foam, and combination of multiple methods have been focused to improve the instantaneous rate of heat transfer. Table 1 shows the comparison of various methods.

Water droplet is an effective form of heat transfer due to the high heat capacity of water and the high surface area of sprays of droplets. So water spray can significantly improve rate of heat exchange, and can be used alone or in conjunction with other methods with solid or liquid piston. For a low compression ratio of two, experimental results show that spray cooling can increase compressor efficiency into the range of 88-97%. To obtain an accurate heat transfer process model, the area of water mist heat transfer in the cylinder are divided into two parts, and the spray angle and nozzle diameter are considered [9]. Odukomaiy *et al.* [10] used spray cooling to achieve near isothermal compression and the system round-trip efficiency is up to 82% and the energy density is 3.59 MJ/m<sup>3</sup>. The performance of a water spray cooling system was investigated by experimentally and theory [11].

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Table 1. Comparison of various near transfer methods								
Method	Instantaneous rate of heat transfer	Advantage	Disadvantage					
Liquid piston	Less than 1000 W/m <sup>2</sup> K [12]	Good sealing performance and no pollution	Air will inevitably dissolve into liquid which leads hydraulic system elastic modulus decreases, and a series of problems such as noise, vibration and cavitation in the low pressure area occurs [13]					
Water spray	Heat transfer coefficients of droplets with diameters of 20 μm and 50 μm are 6000 W/m <sup>2</sup> K and 5000 W/m <sup>2</sup> K [14]	Faster heat exchange rate and being clean and pollution-free to the environment	Certain amount of energy to make water spray [14]					
Liquid piston and water spray	More than 5000 W/m <sup>2</sup> K [15]	Good sealing performance and faster heat exchange rate	Air is dissolved in liquid, resulting in energy waste and high energy consumption in making water spray [13]					
Liquid piston and porous media	N.Anot available	Faster heat exchange rate	Porous media has high cost and occupies a certain volume, which has a certain impact on compression; air dissolves in liquid, resulting in energy waste [16]					
Aqueous foam	N.Anot available	Large heat exchange area and fast heat exchange rate	Difficult to make water foam, and it cannot be fully converted into air and water after heat exchange [17]					

<b>Fable 1. Comparison o</b>	f various hea	it transfer	methods
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Most previous studies of near-isothermal CAES focused on spray cooling system. Few studies focus on spray heating system. In fact, spray heating needs to be applied during expansion process to achieve near-isothermal expansion. Zhang *et al.* [18] conducted a numerical study on the spray heating expansion process and found that it is 12% higher than the adiabatic expansion work. To realize the isothermal expansion process of piston expander, Qihui *et al.* [19] proposed a method to inject micron water mist at high temperature into the cylinder. Simulation results showed the average air temperature in cylinder increased by 24.7%. But the output power/efficiency of the expansion process is reduced by 7.7%/12.3%.

Though the previous studies have considered many aspects, they lack some experimental study of parameters influence especially for the expansion process. Additionally, there is also a lack of experimental studies of the effect of droplet size, spray time. The results of previous numerical studies are inconsistent. Previous studies on near-isothermal CAES have focused on analyzing droplet heat transfer and the compression/expansion process separately, taking into consideration multiple factors such as droplet size, flowrate, pressure ratio, cycle frequency, and chamber configuration. However, up to now, the design and optimization nearisothermal CAES system is a challenging task based on spray. The main objectives of this study was to further investigate the relationship between spray parameters including the spray closing time, the spray opening time, and the nozzle diameter and pressure in cylinder during compression/expansion process of a isothermal compressed air energy system using experimental results. The experimental results is valuable to further investigate and optimize the near-isothermal CAES system based on spray transfer.

This is the first paper to the authors' knowledge to investigate the relationship between the spray parameters and pressure in cylinder during compression/expansion process using experimental results. Importantly, this is the first paper to identify the spray closing time and the spray opening time as the key spray parameters for compression/expansion process of a nearisothermal compressed air energy system. Furthermore, the spray closing time and the spray opening time was optimized based on specific experimental conditions. Thus, it fills an important gap in the literature, as would be need to implement near-isothermal CAES based on spray transfer.

### **Experiments**

### Experimental apparatus and procedure

Figure 1 shows the schematic of the near-isothermal CAES system, which is composed of a compression system, a spray generator system, an expansion system, and a data acquisition system.

Water droplets are sprayed into the compression chamber or expansion chamber which enhances the heat transfer from the air to the surrounding water. The water in the constant temperature container also provides a large heat sink during the operation of the compressor or expander. The inlet and outlet solenoid valves are installed in the passage connected to the compression chamber and expansion chamber. A water mist generator is used to control the supply of water mist inside the compression/expansion chamber. The pressure of the water mist can be adjusted by the water mist generator, and the temperature of the water was controlled by a constant temperature tank. Spray size can be adjusted by changing different nozzles. A programmable logic controller (PLC 200 smart) is used to control the operation of solenoid valves.

The experimental apparatus shown in fig. 2. consists of servo motor (MDME202GCG) by Panasonic, an electric actuator (SDG63-006) by Shanghai Yinghao electromechanical Equipment Co., LTD, two stainless-steel pressure transducer which uses high accuracy silicon sensor (PR-25,  $0\sim1$  MPa,  $\pm0.5\%$  FS) by Keller, two *K*-type thermocouples (pt100,  $0\sim100$  °C,  $\pm1.5$  °C) by MEACON, a magnetic railing ruler (MB500-10-0.05-ST, linear error  $\pm35 \ \mu$ m) by SIKO, a water mist separator by SMC, two high pressure atomizing nozzle by Shenzhen Hanbo Environmental Protection Equipment Co., LTD, an air storage tank by SMC, a constant temperature equipment (DHC-05-A, 0-99.9 °C, Temperature fluctuation



**Figure 1. Schematic of the experimental apparatus;** *1* – *water tank,* 

- 2 constant temperature box,
- 3 water mist generator,

4, 8, 17, 21 2/2 – solenoid valve, 5, 7 – water mist separator, 6 – air storage tank, 9 – muffler,

- 10– flowmeter, 11 check valve,
- 12, 25 2/3 solenoid valve, 13,
- 19 pressure sensor, 14 temperature sensor,
- 15 atomizing nozzle, 16, 18 nozzle,
- $20-expansion\ cylinder,$
- 22 compression cylinder, 23, 26 piston rod,
- 24 coupling, 27 magnetic railing ruler,
- 28 electric actuator, 29 servo motor,
- *30 data acquisition device card, and*
- 31-computer

 $\pm 0.2$  °C) and water tank (5 L) by Hangzhou Qiwei Instrument Co. LTD, a water mist generator (PC-2801, flow rate 0.3 Lpm) by Suzhou HAIGINT electromechanical Co. LTD.

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**Figure 2. Experimental platform photographs;** 1 – servo motor, 2 – electric actuator, 3 – coupling, 4 – compression cylinder, 5 – pressure sensor, 6 – temperature sensor, 7 – computer, 8 – magnetic railing ruler, 9 – water mist separator, 10 – expansion cylinder, 11 – nozzle, 12 – air storage tank, 13 – temperature sensor, 14 – constant temperature equipment, 15 – water tank, and 16 – water mist generator

Pressure sensors are installed at the bottom dead center of the compression chamber and expansion chamber to measure the instantaneous pressure of the air during the compression process and expansion process. Two *K*-type thermocouples are placed inside the compression chamber and expansion chamber to measure the instantaneous temperature of the air. The struc-



Figure 3. Structure diagram of the spray nozzle installation

the instantaneous temperature of the air. The structure of the atomizing nozzle is described in the previous literature of the research group [20]. Figure 2 shows pictures of this study's quasi-isothermal CAES system set-up. The compression chamber and expansion chamber are modified based on existing pneumatic cylinder. So, the diameter and height of the compression chamber are 100 mm and 150 mm, respectively, and the diameter and height of the expansion chamber are 100 mm and 125 mm, respectively.

A Labview program was used to program the operation of solenoid valves. Instantaneous pressure and temperature data during compression and expansion cycles are recorded using a data acquisition device through the LabVIEW program. The measurement devices were calibrated repeatedly to maintain measurement accuracy.

Spray nozzles are attached to the bottom of the compression chamber and expansion chamber to generate spray inside the chamber as shown in fig. 3.

#### Parameter definition

In the present study, we first studied the influences of the spray system on the compression and expansion process. Then the influences of the spray time and the nozzle size on the pressure in the compression or expansion chamber were investigated subsequently while keeping other operating parameters invariable. The nozzle inlet heating or cooling degree was precisely controlled. The spray time can be adjusted by program control. To change the nozzle size, different types of nozzles were applied. To study the effect of spray time, the spray opening time and closing time need to be defined based on compression process.

$$t_{op} = \frac{y_{so}}{v} \tag{1}$$

$$t_{cl} = \frac{y_{sc}}{v_{p}}$$
(2)

where  $y_{so}$  is the position of the piston when the spray control valve is energized,  $y_{sc}$  – the position of the piston when the spray control valve is de-energized, and  $v_p$  – the velocity of the piston.

The compression ratio,  $R_p$ , is described as:

$$R_p = \frac{V_{ic}}{V_c} \tag{3}$$

where  $V_{ic}$  is the initial air volume of compression chamber and  $V_c$  – the volume of air being compressed.

The expansion ratio,  $R_{ex}$ , is defined by:

$$R_{ex} = \frac{V_{ie}}{V_e} \tag{4}$$

where  $V_{ie}$  is the initial air volume of expansion chamber and  $V_e$  – the volume of supply air during expansion process.

The schematic of the piston movement during the compression process and expansion process can be shown in fig. 4. The initial position of the piston is the top dead center (TDC). The final position of the piston is the bottom dead center (BDC).

#### Experimental results and discussion

#### Influence of spray system

During the process of experiment, the environment pressure, environment temperature are 0.1 MPa and 293 K, respectively. To obtain the influence of the spray system, with and without water spray experiment were performed during the compression process and expansion process. The experimental conditions are summarized in tab. 2.

During the compression process, the spray inlet pressure is set to 2 MPa, and the inlet water temperature is kept at 288 K. The diameter of the nozzle is 0.6 mm. The solenoid valve



which controls the water spray is energized when the air starts to compress by the piston. When the piston reaches the BDC, the solenoid valve is de-energized. The velocity of the piston is equal to 0.1 m/s. During the expansion process, the spray inlet pressure is set to 6 MPa, and the inlet water temperature is kept at 363 K. The diameter of the nozzle is 0.8 mm. The compressed air flows into the expansion chamber, meanwhile, the water is sprayed into the expansion chamber until the piston reaches the BDC.

Case	Parameters	Value
	Diameter of compression cylinder, $D_{cy}$	100 mm
Compression process without water sprey	Stroke of compression cylinder, <i>S</i> <sub>cy</sub>	150 mm
Compression process without water spray	Compression ratio, $R_p$	2
	Velocity of piston, <i>v</i> <sub>p</sub>	0.1 m/s
	Compression ratio P	2
	Velocity of niston $v_n$	0.1 m/s
	Spray pressure, $p_{sw}$	2 MPa
Compression process with water spray	Diameter of nozzle, $D_{nc}$	0.6 mm
	Spray opening time, <i>t</i> op	0 seconda
	Spray closing time, $t_{cl}$ Water mist temperature, $T_{mc}$	1.2 seconds
		288 K
	Expansion cylinder diameter. Dev	100 mm
	Expansion cylinder stroke, $S_{ev}$	125 mm
Expansion process without water spray	Expansion ratio, $R_{ex}$	3
	Intake pressure, $p_s$	0.4 MPa
	Intake air temperature, $T_s$	293 K
	Expansion cylinder diameter, $D_{ey}$	100 mm
	Expansion cylinder stroke, Sey	125 mm
	Expansion ratio, $R_{ex}$	3
	Intake pressure, <i>p</i> <sub>s</sub>	0.4 MPa
Expansion process with water spray	Intake air temperature, $T_s$	293 K
	Diameter of nozzle, $D_{ne}$	0.8 mm
	Spray pressure, <i>p</i> <sub>sp</sub>	6 MPa
	Water mist temperature, $T_{we}$	363 K

 Table 2. Experimental conditions

Variations of the pressure in the compression chamber and expansion chamber with spray and without spray are shown in fig. 5.



Figure 5. Variation of pressure; (a) compression chamber and (b) expansion chamber

From fig. 5(a), we can see that whole compression process can be described by the following processes:

- The A-B curve denotes the suction stage. In this stage, the pressure in the compression chamber decreases owing to the piston's upward leading to the volume of the chamber increase.
- The B-C curve denotes the stable stage. In this stage, the pressure in the compression chamber keeps constant pressure.
- The C-D curve denotes the compression stage. The pressure in the compression chamber sharply increases owing to the piston's rapid downward. In this stage, the water spray at 288 K is injected into the compression chamber. Obviously, the pressure in the compression chamber with spray is lower than that without spray.
- The D-E curve denotes the exhaust air stage. In this stage, the pressure in the compression chamber exhaust into the air storage tank. As the number of cycles increasing, the exhaust pressure gradually increases.

The maximum pressure in the compression chamber is about 0.212 MPa with spray enhanced heat transfer. The maximum pressure in the compression chamber decreases by 19.8% without spray-enhanced heat transfer. This means that the spray-enhanced heat transfer can reduce the work consumption during the compression process.

From fig. 5(b), we can see that the whole expansion process can be expressed by the following process:

- The A-B curve denotes the inlet air stage. In this stage, compressed air flows into the expansion chamber and the pressure in the expansion chamber increases.
- The B-C curve denotes the expansion process. The intake valve is closed. The compressed air continues expansion and the pressure in the expansion chamber decreases. In this stage, the water spray at 363 K is injected into the expansion chamber. It is obvious that the pressure in the compression chamber is higher with spray than without spray.
- The C-D curve denotes the exhaust process. In this stage, the exhaust valve is opened. The
  residual compressed gas exhausts into the environment by piston drive.

Generally, the area contained in the p-V diagram is regarded as output work. It is obvious that the output work with spray enhanced heat transfer is larger than without spray enhancing heat transfer.

# Influence of spray closing time and opening time during compression process

Based on the experimental platform, the maximum stroke of the compression cylinder is 150 mm.

The velocity of the piston's movement is equal to 0.1 m/s. It takes the piston from the TDC to the BDC spends 1.2 seconds. When the position of the piston is at the TDC and starts to compress, the moment is defined as the initial moment. The fig. 6(a) shows the relationship between spray closing times and the maximum air pressure in the compression chamber under with a compression ratio of 2.



(a) different spray closing time and (b) different spray opening time

It can be seen from the fig. 6(a) that the changing trend of the gas pressure in the cylinder obtained by the experiment at differences spray closing time. The maximum air pressure of gas in the compression chamber will remain unchanged after the spray closing time is 0.6 seconds, and will only increase when it is less than 0.6 seconds. This shows that the mass of water mist injected at the stage of 0.6-1.2 seconds at the time of spray closing is excessive, and the heat exchange between water mist and air is not affected by closing the water mist in advance. With the closing time of spray less than 0.6 seconds, the mass of sprayed water mist is less than the saturation value, and there is not sufficient heat exchange with air, so the gas pressure increases due to limited heat exchange.

It can be seen from the fig. 6(b) that the changing trend of the gas pressure in the cylinder obtained from the experiment at different spray opening times. The pressure of gas in the compression chamber increases with the increase of spray opening time and remains unchanged after 0.6 seconds, which shows that spraying water mist within 0.6-1.2 seconds has no heat exchange effect on the air in the cylinder. Therefore, spraying water mist into the compression chamber after 0.6 seconds will not reduce the gas pressure inside the cylinder and will not improve the compression efficiency of the system.

## Effect of spray size

The compression ratio is set to 2, the piston speed is set to 0.1 m/s, and the compression experiments are carried out under different nozzle diameters, and the nozzle diameters are 0.3 mm, 0.5 mm, and 0.8 mm, respectively. It can be seen from the fig. 7(a) that spraying water mist particles with different nozzle diameters in the compression chamber has certain influence on the heat transfer effect between water mist and air. When the nozzle diameter is 0.3 mm, the maximum pressure in three compression cycles is 0.223 Mpa. When the nozzle diameter is 0.5

mm, the maximum pressure in three compression cycles is 0.217 Mpa. When the nozzle diameter is 0.8 mm, the maximum pressure in three compression cycles is 0.211 MPa. Therefore, it can be concluded that the smaller the nozzle diameter is, the better the heat exchange capacity of water mist is.



(b) expansion chamber

In order to obtain the specific changes of the air pressure in the cylinder under the fixed intake pressure and the fixed spray pressure, experiments were conducted with nozzle diameters of 0.3 mm, 0.5 mm, and 0.8 mm, respectively, and the experimental study was carried out when the intake pressure was 0.4 MPa, the water temperature was 363 K, and the spray pressure was 6 MPa. It can be seen from the fig. 7(b) that the relationship between the specific changes of the air pressure in the cylinder. During the expansion process, the energy from water spray is injected into the expansion chamber. The larger the nozzle diameter is, the more water flows into the expansion chamber. So if we ignore the energy consumption of spray system, the larger the nozzle diameter is, the more the expansion output is.

### Conclusions

The CAES system based on spray enhanced heat transfer is investigated. The influence of spray system, spray closing time, spray opening time and the diameter of the nozzle are studied experimentally. Based on thorough experiments the following conclusions can be drawn:

- Under same conditions, CAES system with spray heat transfer system can reduce the work consumption during the compression process compared with without spray heat transfer system. And during the expansion process, the output work will increased due to high temperature water spray injected into expansion chamber.
- For the same nozzle, the spray closing time and opening time have the critical value to decrease the maximum air pressure during compression process. Under the given condition, the critical spray closing time and opening time are 0.6 seconds, and 0.6 seconds, respectively.
- To compression process, the reduction of nozzle diameter can decrease maximum air pressure in compression chamber.
- To expansion process, if the energy consumption is ignored, the larger the nozzle diameter, the greater the expansion output.

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### **Conflicts of Interest**

The authors declare no conflict of interest or personal relationships that could have appeared to influence the work reported in this paper.

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