TRANSITIONAL FREE CONVECTION FLOW AND HEAT

by

TRANSFER WITHIN ATTICS IN COLD CLIMATE

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The transitional free convection flow and heat transfer within attics in cold climate are investigated using 3-D numerical simulations for a range of Rayleigh numbers from 10^3 to 10^6 and height-length ratios from 0.1 to 1.5. The development process of free convection in the attic could be classified into three-stages: an initial stage, a transitional stage, and a fully developed stage. Flow structures in different stages including transverse and longitudinal rolls are critically analyzed in terms of the location and strength of convection rolls and their impacts on the heat transfer. The transition unsteady flow and asymmetry flow in the fully developed stage is discussed for the fixed height-length ratio 0.5. Various flow regimes are given in a bifurcation diagram in the parameter space of Rayleigh numbers ($10^2 < Ra < 10^7$) for heightlength ratios (0.1 < A < 1.5). The time series of heat transfer rate through the bottom wall is quantified for different height-length ratios. The overall heat transfer rate for the low Prandtl fluid (Pr = 0.7) could be enhanced based on 3-D flow structure.

Key words: transitional flow, Rayleigh number, convection roll, height-length ratio, attic space

Introduction

Thermal convection is an important mechanism of flow and heat transfer in nature and technology [1-7]. The work about thermal flows in attics is of basic meaning for the realizing of thermal convection system, and also of actual significance for the architecture of thermal comfort in buildings. A number of research works have been devoted to free convection and heat transfer in attics [8-11].

The flow in attics is potentially unstable for the cold climate. The experiment showed that transitional convection flows may proceed at a high Rayleigh number, under the cold climate [12, 13]. Additionally, the relation between the Nusselt number and the height-length ratio at various Rayleigh numbers was quantified [14-16]. They also obtained some elementary

4699

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scales of transient free convection [17]. As the Rayleigh number increases, the free convection flow in the attic space experiences a transitional process from symmetry to asymmetry phenomenon in the cold climate [18, 19].

Multiple states occurred in attics for the cold climate involving two different fluids (Pr = 0.7 and Pr = 7). Lei *et al.* [20, 21] conducted the schlieren experiment with the water fluid medium. Cui *et al.* [22] simulated the development process of free convection flows with Pr = 7 in the section-attic cavity in the cold climate in a wide range of Rayleigh numbers [23, 24]. These 3-D studies aforementioned are focused on the water medium. How does Prandtl number affect the appearance of multiple flow states. Are there numerous steady-states exist for the air medium (Pr = 0.7). What is the role of Rayleigh number and height-length ratio on the symmetry spoiling phenomenon leading to asymmetric flow for the air medium? However, the research on the aforementioned questions is not very clear.

Our work attempt to clarify the problems for free convection within the attic space for the cold climate. In this numerical research, the transient development of free convection in attic space is observed for $Ra = 10^6$. The infulence of Rayleigh number on 3-D flow, asymmetry and unsteady flow is researched. We also considered the effect of height-length ratio. The research is expected to provide ideas for building thermal design and achieve the purpose of energy saving.

Computational model and procedure

The physical system consisted of an attic space of height H, length 2L, and depth W full of air medium as illustrated in fig. 1. The inner walls of the attic are set as non-sliding walls. Initially, the temperature of air in the attic was T_0 . At an initial time, the bottom wall is heated and keeps it at a higher temperature T_h , while the two top walls are cooled and stay at a lower temperature T_c . The other two vertical walls are insulated. We assumed that the medium behaves as an ideal gas. The thermal conductivity, κ , specific heat capacity, and viscosity are set as con-



Figure 1. Schematic diagram of computational domain and boundary conditions for A = 0.5 [22]

$$T_0 = (T_{\rm h} + T_{\rm c})/2$$
. It have been demonstrated that
3-D Navier-Stokes equations and energy equa-
tion with Boussinesq approximation could de-
scribe well free convection in attics. The scales
are summarized x, y, $z \sim H$; $t \sim H^2/(\kappa Ra^{1/2})$;
 $(T-T_0) \sim (T_{\rm h} - T_c)$; $u, v, w \sim \kappa Ra^{1/2}/H$; and $\rho^{-1}\partial p/\partial x$,
 $\rho^{-1} \partial p/\partial y$, $\rho^{-1}\partial p/\partial z \sim \kappa^2 Ra/H^3$. The non-dimen-
sional governing equations are expressed:

stants and calculated at the reference temperature

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \tag{1}$$

$$\frac{\partial u}{\partial t} + u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = -\frac{\partial p}{\partial x} + \frac{\Pr}{\operatorname{Ra}^{1/2}} \left(\frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right)$$
(2)

$$\frac{\partial v}{\partial t} + u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = -\frac{\partial p}{\partial y} + \frac{\Pr}{\operatorname{Ra}^{1/2}} \left(\frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right) \Pr T$$
(3)

$$\frac{\partial w}{\partial t} + u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} = -\frac{\partial p}{\partial x} + \frac{\Pr}{\operatorname{Ra}^{1/2}} \left(\frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right)$$
(4)

Cui, H., *et al.*: Transitional Free Convection Flow and Heat Transfer Within ... THERMAL SCIENCE: Year 2022, Vol. 26, No. 6A, pp. 4699-4709

$$\frac{\partial T}{\partial t} + u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} + w \frac{\partial T}{\partial z} = \frac{1}{\mathrm{Ra}^{1/2}} \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} + \frac{\partial^2 T}{\partial z^2} \right)$$
(5)

It is expected that free convection flows and heat transfer in attics were controlled by three non-dimensional numbers: the Rayleigh and Prandtl numbers and the height-length ratio, A, [25], which are defined:

$$Ra = \frac{g\beta(T_{h} - T_{c})H^{3}}{\nu\kappa}, Pr = \frac{\nu}{\kappa}, A = \frac{H}{L}$$
(6)

Finite volume method was used to solve the governing eqs. (1)-(5), and the pressure-velocity coupling problem was solved by using the SIMPLE scheme. Table 1 showed results of mesh and time step dependence experiments for A = 0.5. We also do similar grid and time step tests for other models with various ratios and Rayleigh number. Here, we will define the mean Nusselt number in the quasi-steady stage as [17]:

$$Nu = \frac{1}{S} \iint_{S} Nu_{local} \, dS \tag{7}$$

Three different non-uniform and symmetric meshes $(L \times H \times W)$ 110×30×41, 141×41×51, and 171×51×61 and two time steps 0.01 and 0.02 were tested. In order to balance the problem of calculation cost with the accuracy of results of different grids and time steps, the grid of 141×41×51 cells and the time step of 0.02 were adopted in this work.

For further verification, the numerical simulation results of the work are compared with the antecedent experiments in [18], which is shown in fig. 2. Clearly, the computational result agree well with the experimental result in fig. 2(b) in [17]. The quantitative contrast between the numerical test and other published experimental test [13] is also carried out as seen in fig. 3. At the same position, the temperature difference is less than 10%.

Table 1. Correlation test results of mesh and time step for A = 0.5

1		
$Mesh \\ L \times H \times W$	Time step	Ra = 10 ⁷ Variation of Nu [%]
$110 \times 30 \times 41$	0.02	1.75
141×41×51	0.02	_
171×51×61	0.02	0.41
141×41×51	0.01	0.30



Figure 2. The comparison of numerical and experimental results [14] for Ra = $7 \cdot 10^4$ and A = 0.5; (a) numerical flow pattern and (b) experimental flow pattern

Figure 3. Contrast between numerical test and the published experimental result [13] for Ra = $2.2 \cdot 10^5$, A = 1and Pr = 0.7



4701



Figure 4. Time series of Nusselt number for different Prandtl numbers, A = 0.5 and Ra = 10⁶ (the red dash dot line is for Pr = 7 [22]; the black solid line is for Pr = 0.7

Transition of free convection flows Transient development of nature convection

The development of transient nature convection for Pr = 0.7 consists of an early, a transitional and a fully development stage, as shown in fig. 4, which is similar to that for Pr = 7 [22]. The initial stage becomes shorter, and the transitional stage exists earlier and lasts for a long time more than 10 seconds. The Nusselt number for Pr = 0.7 has larger oscillation and approximately twice than that for Pr = 7 in the quasi-steady stage.

What is the difference of flow structures in different stages for different Prandtl numbers. As shown in fig. 5(a), the characteristics of the flow in the early stage is the formation of a thermal boundary-layer around the wall surfaces. During transition stage, the intrusion flow near the bottom surface begins to form at t = 8, as shown in fig. 5(b). Oppositely moving intrusion streams



Figure 5. Temperature iso-surfaces at different times for Ra = 10^6 and A = 0.5; the bule temperature iso-surface is T = -0.3, the red temperature iso-surface is T = 0.3; (a) t = 2, (b) t = 8, (c) t = 25, and (d) t = 2800

Effect of Rayleigh numbers

In fig. 5(b). Oppositely moving intrusion streams meet to form upward moving thermal plumes. We can find that the heated plumes ascend in the middle of the attic, and cooled plumes descend near the tip region from fig. 5(c). Compared with the large Prandtl number fluid, the small Prandtl number fluid develops slowly [23, 24]. In fully developed stage, the flow is unsteady and 3-D, which is more complex than that for Pr = 7. The flow characteristics in the quasi-steady stage will be discussed in the following portion on the basis of the observation of numerical simulation results.

For small Rayleigh numbers, the temperature field is stratified, and there are two symmetric transverse rolls in the flow field, as seen in fig. 6. For $Ra = 10^4$, the isotherms are no longer parallel, and one transverse roll increases and moves toward the center. The short longitudinal rolls form near the tip of the bottom. As Rayleigh number goes up, the 3-D flow characteristics become more obvious. The longitudinal rolls exist over the entire bottom surface.



Figure 6. Temperature iso-surfaces and streamlines in the attic space at t = 2800 in the quasi-steady stage for A = 0.5. The bule surface is the temperature iso-surface of T = -0.3, the red surface is the temperature iso-surface of T = 0.3

The difference of flow configuration in the full development stage shows that the evolution from approximately 2-D to 3-D and from symmetry to asymmetry. The following paragraphs will describe the convective rolls, asymmetric flows and unsteady flows in the evolutionary stage.

Onset of convection rolls

We will observe the convection rolls from different sections of the attic space. When the Rayleigh number is low (Ra = 10^3), the temperature structure of the air in the attic is stratified, and the thermal boundary-layer shape (from T = -0.5 to T = -0.4) is very clear in fig. 7. The flow is driven by buoyancy force near the inclined wall, and the flow is in the state of steady laminar and its intensity is weak. The weak basic flow is considered as a 2-D flow in the attic space.



Figure 7. Isotherms and streamlines in the *xy*-cross-section at different locations in the fully developed stage (t = 2800) for A = 0.5

As Rayleigh increases ($Ra = 10^4$), one of transverse rolls increases in size and move toward the middle of the attic. Another transverse roll remains but diminishes in size. The secondary transverse roll forms in the corner region near the large convective roll. The apparent asymmetry is clearly different from that of water medium [23, 24]. When Rayleigh number further increases above the critical value, the flow patterns become more asymmetric and the number of secondary vortices have a tendency to increase. For Ra = 105, the secondary transverse roll breaks up and occupys the entire tip region.

At $Ra = 10^6$, the asymmetry phenomenon is obvious. The secondary transverse rolls increase in number, appear throughout the attic space and superimpose on two large transverse rolls. These transverse rolls have reduced length and irregular shape. In this case, the boundary-layers at the region of inclined surface and bottom surface become thinner.

In order to observe longitudinal rolls, fig. 8 shows isothermals and streamlines in different yz-cross-sections with Rayleigh number from 10^3 to 10^5 . For Ra = 10^3 , they are similar to those for the water medium, see [25-27] for details. As Rayleigh number increases, weak cells appear nearby two vertical walls in the yz-cross-section (x = 0.5) when Ra = 10^4 . With the Rayleigh number further development, longitudinal rolls appear near the vertical sidewalls, as seen in the yz-cross-section (x = 1) for Ra = 10^5 . The length of longitudinal rolls is not large, because the longitudinal rolls don't exist in the plane x = 1. The horizontal flow at the bottom of the region, creating longitudinal convection rolls, like the formation mechanism of Rayleigh-Benard-Poiseuille flow [20]. However, the longitudinal rolls in attics are more irregular in shape than that for the water medium, especially for higher Rayleigh numbers.



Figure 8. Isotherms and streamlines in the *yz*-cross-section at different locations in the fully developed stage (t = 2800) for A = 0.5

Figure 9 shows dependence of the averaged vorticity for different Rayleigh numbers. We define the mean vorticities in x-, y-, and z-direction in the quasi-steady stage as [21]:

$$\Omega_{x} = \frac{1}{V} \iiint_{V} \left| \frac{\partial w}{\partial y} - \frac{\partial v}{\partial z} \right| dV$$
(8)

$$\Omega_{y} = \frac{1}{V} \iiint_{V} \left| \frac{\partial w}{\partial x} - \frac{\partial u}{\partial z} \right| dV$$
(9)

$$\Omega_{z} = \frac{1}{V} \iiint_{V} \left| \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right| dV$$
(10)

$$Q_{t} = Q_{x} + Q_{y} + Q_{z} \tag{11}$$

where we can use the vorticity of Ω_x , Ω_t , and Ω_z to quantitatively describe longitudinal rolls, transverse rolls and total rolls, respectively, also see [21]. When Rayleigh number is less than 10³, the magnitude of vorticity is almost zero. The onset of Rayleigh-Benard convection rolls lead to an increase in vorticity Ω_z around $Ra_{TR} = 10^3$ for A = 0.5. Moreover, the critical Rayleigh number at the start of longitudinal rolls is about $Ra_{LR} = 1.3 \cdot 10^4$, which is smaller than that for the water medium. The strength of the total rolls significantly increase around $Ra = 3 \cdot 10^4$, and the value of Ω_z is lower than that for the water medium.



Transition asymmetry flow

The asymmetry flow in the attic space is obvious in fig. 7. As a results of pitchfork bifurcation, the transition from symmetry to asymmetry flows around the geometric central plane appears [19, 21, 22, 25]. As defined in the previous study [19], the asymmetry flow in the attic is calculated use the degree *I*:

$$I = \frac{\iiint_{V} \left[T(x, y, z) - T(-x, y, z) \right]^{2} dV}{4 \iiint_{V} \left[T(x, y, z) \right]^{2} dV}$$
(12)

Figure 10 shows the values of *I* with different Rayleigh numbers at range of $Ra = 10^2$ to 10^7 . Clearly, *I* significantly increases around $Ra_I = 9 \cdot 10^3$. This implies that the critical Rayleigh number Ra_I from symmetry to asymmetry flows is smaller than that for the water medium. The value of I quantifying the asymmetry flow is almost 3-orders higher than that of water medium.

Transition oscillatory convection

In this section, the height-length ratio of the attic is 0.5. The numerical results show that there is no oscillation in the states of the three transverse rolls at $Ra = 3 \cdot 10^4$. The temperature at the monitoring points in fig. 11(a) has not changed over time. Small perturbations appear in the temperature time series at Rayleigh number $3.4 \cdot 10^4$, as illustrated in fig. 11(b). The meaning is the transition from steady to unsteady flow state occurs around $Ra_{US} = 3.4 \cdot 10^4$.

For observing the characteristics of unsteady flow and demonstrate its transition turbulence, fig. 11(c) shows the power spectrum density (PSD) of the periodic flow in the full development stage for Ra = $3.4 \cdot 10^4$, and the main frequency ($f_p = 0.0004$) and harmonic frequencies are clear. The peak frequency on the spectrum is consistent. As the Rayleigh number increases, the flow is still periodic, but the peak frequency changes with $f_p = 0.0011$ at P1 and $f_p = 0.0005$ at P3(P3') for Ra = $4 \cdot 10^4$, see figs. 11(d)-11(e). In addition, subharmonic frequencies appear in the spectrum diagram.

The chaotic flow appears near $Ra = 5 \cdot 10^4$. The temperature time series and the corresponding PSD are plotted in figs. 11(f)-11(g). There is no clear dominant peak frequency and harmonic frequency in this mode. This indicates that the flow occurs chaotic. The Rayleigh number of flow transition chaos in the attic with water medium is one order of magnitude higher than that of air medium. Current studies show that the change of Prandtl number has a signif-



icant effect on the critical Rayleigh number of flow evolution, its construction, frequency time evolution and space evolution.

Figure 12. A state diagram of the observed patterns in triangular cavities with different Rayleigh numbers and height-length ratios and Pr = 0.7; Region I is the 2-D symmetrical steady flow, Region II is the 3-D symmetrical steady flow, Region III is the 3-D asymmetrical steady flow, Region IV is the 2-D asymmetrical steady flow and Region V is the 3-D asymmetrical unsteady flow



and PSD of the convection at P1 (0, 0.5, 1), P3 (-0.54, 0.11, 1), P3' (0.54, 0.11, 1) with different Rayleigh numbers; (a) Ra = $3 \cdot 10^4$, (b) Ra = $3.4 \cdot 10^4$, (c) Ra = $3.4 \cdot 10^4$, (d) Ra = $4 \cdot 10^4$, (e) Ra = $4 \cdot 10^4$, (f) Ra = $5 \cdot 10^4$, and (g) Ra = $5 \cdot 10^4$

Flow regime

According to the aforementioned analysis, it can be obtained that the 2-D symmetric steadystate firstly appears in the triangular attic under low Rayleigh numbers, as shown in Region I in fig. 12. Region I can be divided into a basic flow region. The flow in this region is driven by the fluid near the cooling inclined walls and forms two symmetrical transverse convective rolls with opposite rotational directions. As Rayleigh number increases, the Rayleigh-Benard instability strengthens the intensity of the transverse convective rolls, and the instability in the triangular attic with the lower height-length ratio makes the convective rolls bifurcating into many pairs.

For small height-length ratio (A < 0.5) and large height-length ratio (A > 1.1) of the attic (Region II), followed by the 3-D asymmetric steady-state (Region III). The 3-D flow in the attic with small height-length ratio is mainly the longitudinal convective rolls, while the 3-D flow in the attic with large height-length ratio is mainly the Rayleigh-Benard convective cell. With the increases of Rayleigh number in the attic that the height-length ratio between 0.5 and 1.1, the flow firstly presents a 2-D asymmetrical steady-state (Region IV), and then a 3-D asymmetrical steady-state (Region III).

For all height-length ratios, as the Rayleigh number continues to grow, the flow in attics presents a turbulent state, as shown in Region V. The critical Rayleigh number of this state is positively correlated with the height-length ratio.

Heat transfer

As the height-length ratio increase, the evolution tendency of Nusselt number over time is similar, seen in fig. 13. However, the time reaching the quasi-steady-state is gradually delayed, and the value of Nusselt number gradually is increased. In the fully developed stage, the fluid-flow is unsteady for A = 0.1 and 0.2. For the attic with smaller height-length ratio, the flow reaches an unsteady-state at lower Rayleigh number.

As shown in fig. 14, the Nusselt number of the bottom surface is slightly larger than that of the top surface, which is analogous to the 2-D simulation result [21]. The Nusselt number increases as the Rayleigh number increases. How does the Nusselt number change with Rayleigh number. The fitting results of 3-D numerical simulations are higher than Nu ~ Ra^{1/3}, which is accordance with the heat transfer law in Rayleigh-Benard convection [28, 29]. This maybe caused by the existence of longitudinal convection rolls in the attics.



Conclusions

This paper focuses on the evolution of different flow states and their impact on the physics of heat transfer in attics. The transient stages are relatively earlier than those for the water medium. In the quasi-steady stage, the 3-D flow structures in the quasi-steady stage depend on what the Rayleigh number is. These Rayleigh numbers including Ra_{TR} , Ra_{LR} and Ra_I are lower than those for the water medium. Nevertheless, the asymmetry phenomenon is more obvious due to the large-scale movement of the transverse rolls. The transition an unsteady flow state largely depends on the appearance of 3-D flow. The critical Rayleigh number of the unsteady phenomenon in the attic space is significantly lower than that for larger Prandtl number. In the Ra-A regime diagram, the 2-D asymmetrical steady flow state exists, which is not observed in other studies. Heat transfer rate in attic space increase as the height-length ratio and Rayleigh number increase. The relation between Nusselt and Rayleigh numbers is higher than Nu ~ Ra^{1/3}. It demonstrates that the flow structure in three dimensions is helpful in heat transfer.

For the first time, the distribution of flow patterns in the attic space has been shown in the control parameter space based on numerical simulation, which has guiding significance for understanding the flow mechanism in the cavity. The variation of heat transfer law in the attic with the aspect ratio and Rayleigh number is given, which is instructive to the thermal design of buildings. Further experimental results of 3-D flow structure in attics will be given in the future.

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Nomenclature

- *A* height-length ratio
- g gravitational acceleration, [ms⁻²]
- H, L, W height, half length, and
 - width of the attic, [m]
- Nu Nusselt number
- Nu_b Nusselt number of the bottom
- Nu_{local} local Nusselt number of the surface
- Nu_t Nusselt number of the top
- n co-ordinate normal to the wall
- *p* non-dimensional pressure
- Pr Prandtl number
- Ra Rayleigh number
- Ra₁ critical Rayleigh number for appearance of the asymmetry flow
- Ra_{LR} critical Rayleigh number for appearance of longitudinal rolls
- Ra_{TR} critical Rayleigh number for transverse rolls dominated by RB convection
- Ra_{US} critical Rayleigh number for appearance of the unsteady flow

- S area of the wall, $[m^2]$
- *T* non-dimensional temperature
- T_0 initial temperature(K)
- $T_{\rm c}, T_{\rm h}$ temperatures of the cold inclined top and the hot bottom, [K]
- t non-dimensional time scale
- u, v, w non-dimensional x-, y- and z-velocity
- V volume of the attic, [m³]
- x, y, z non-dimensional co-ordinate

Greek symbols

- β coefficient of thermal expansion, [mK⁻¹]
- κ thermal diffusivity, [m²s⁻¹]
- v kinematic viscosity, [Nsm⁻²]
- ρ medium density, [kgm⁻³]
- Ω_t the total averaged magnitude of vorticity, $[s^{-1}]$
- $\Omega_x, \Omega_y, \overline{\Omega_z}$ the averaged magnitude of vorticity in the *x*-, *y*-and *z*-direction, [s⁻¹]

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Cui, H., et al.: Transitional Free Convection Flow and Heat Transfer Within ... THERMAL SCIENCE: Year 2022, Vol. 26, No. 6A, pp. 4699-4709

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