INCLINED MAGNETIC FIELD EFFECTS ON MARANGONI FLOW OF CARREAU LIQUID

by

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Marangoni convection flow of Carreau liquid by an inclined porous surface is addressed. Magnetic field is taken inclined. Non-linear thermal radiation effects are incorporated considering the Rosseland's approximation. Runge-Kutta-Fehlberg fourth fifth order scheme is utilized to solve the non-linear equations subject to non-linear convective boundary conditions. Non-linear expression of Nusselt number is derived. Concrete graphical description is present out for flow velocity, temperature and Nusselt number. Numerical treatment of non-linear Nusselt number is performed and analyzed.

Key words: Marangoni convection, Carreau liquid, inclined magnetic field, non-linear thermal radiation, inclined surface, numerical solution

Introduction

Marangoni convection arise due to the surface tension gradient in the interfacial liquid-flow. It accelerates the procedures of heat and mass transfer. Such consequence is employed in stabilizing the soap films, drying the silicon wafers in the manufacturing of integrated circuits, self-assembling of the nanoparticles into ordered arrays, semiconductor processing, welding, nucleation, etc. Recently, Zhao et al. [1] carried out Marangoni convection effect in flow of Maxwell fluid. They adopted numerical procedure for the fractional flow model and studied the characteristics of surface tension and heat transfer performance in the flow field. Analysis of Marangoni effect for single-wall (SWCNT) and multi-wall carbon nanotubes (MWCNT) is carried out by Hayat et al. [2]. They found that MWCNT moves fast as compared to the SWCNT and thermal radiation heats up the fluid. Sheikholeslami and Ganji [3] inspected the Marangoni convection effect for forced convection heat transfer of CuO-water nanofluid. They developed the solution using Runge-Kutta integration method and investigated that the Lorentz force reduces the nanofluid's velocity. Discussion on Marangoni convection is made by Aly and Ebaid [4]. They worked on nanofluid with the effects of magnetic field, thermal radiation, suction/injection and porous medium. They deliberate over the physical insight of the flow and observed that the effective electrical conductivity makes a very considerable and remarkable effect on the nanofluids' flow. Hayat et al. [5] developed the analytic solutions for the momen-

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tum and energy equations considering Marangoni convection of Casson fluid. They found the velocity to be an increasing function of mixed convection parameter for assisting flow whereas reverse impact is reported for the opposing flow. The Carreau fluid model lies in the category of generalized Newtonian fluids whose viscosity depends upon the rate of shear. It reduces to the classical Newtonian model when the power law index is numerically equal to 1. This model also overcomes the shortcomings of the power-law model by describing the viscosity for very small/large shear rates. Carreau fluid is attracted by many researchers in literature. Khan et al. [6] examined the Carreau nanofluid-flow in an expanding contracting cylinder with heat and mass transfer processes. They considered the temperature dependent thermal conductivity and computed the numerical results through bvp4c scheme. They considered both the shear thinning and shear thickening cases. Carreau-Yasuda fluid for unsteady squeezed flow model has been considered by Salahuddin et al. [7]. They considered the flow through horizontal sensor surface and numerical solution has been computed by Runge-Kutta-Fehlberg scheme. Hashim and Masood [8] examined the Carreau fluid-flow with Cattaneo-Christov heat transfer effects. They computed the numerical solutions through Runge-Kutta-Fehlberg iterative scheme. They explained that the flow velocity and the temperature were decelerated for higher values of the wall thickness parameter. A peristaltic study of Carreau-Yasuda fluid in a curved conduit is conducted by Abbasi et al. [9]. Flow situation is described through lubrication approach and the properties of Hall effects are discussed in a curved conduit. Flow of Carreau-Yasuda fluid for Hall and MHD effects is examined by Hayat et al. [10]. They considered the curved walls and enlightened the processes of heat and mass transfer. Effectiveness of inclined magnetic field is considered by scientists and engineers for example its role for the stagnation point flow of nanofluid is given by Hayat et al. [11]. They evolved the solutions for momentum, energy and mass transfer equations considering the heat generation/absorption and thermal radiative processes in heat transfer. Khan et al. [12] assumed the oscillatory oblique stagnation point flow for the nanofluid with nanoparticles of copper, alumina, and titania. They calculated the graphical and tabular results for the flow configuration. Sivaraj and Sheremet [13] constructed the solution for viscous fluid-flow in an inclined porous cavity with the effects of inclined uniform magnetic field. They established Brinkman-extended Darcy model and calculated the numerical solutions for different inclinations. An inclined channel is considered by Abbas et al. [14] for two-phase flow of magnetite-water using inclined magneto convection, radiative heat transfer and slip effects. They developed a non-linear differential model and computed the analytic solutions. Shahzadi and Nadeem [15] contributed their work for the nanofluid-flow with an inclined magnetic field effects. The transfer of heat through radiation performs an important role for the engineering mechanisms at high temperatures. Radiative heat transfer also has significant importance in space technology for dealing with solar energy, in polymer industry for the extrusion of polymers, in nuclear industry for controlling the heat transfer mechanism and many engineering processes. Particularly, radiative heat transfer in electrically conducting fluids is more important for the nuclear and industrial engineering purposes for example the design of equipment, gas turbines and several propulsion devices for aircraft missiles, nuclear plants, space vehicles and satellites. The literature reveals that radiative heat transfer is discussed in many researches. Radiative heat transfer study of a Jeffrey viscoelastic fluid with dust-particle suspensions is carried out by Bhatti et al. [16]. They developed the electro-MHD peristaltic flow in planar channel containing a homogenous porous medium. They constructed the analytic solution and discussed the dusty fluid dynamics in detail through graphs and tables. Non-linear thermal radiation effects for thin liquid film with heat source/sink and chemical reaction are discussed by Pal and Saha [17]. They developed the flow over an unsteady porous stretching

surface considering the convective boundary conditions. They used the shooting method together with Runge-Kutta-Fehlberg technique and enlighten the significant parametric effects on velocity and temperature profiles. Hsiao [18] developed the forced and free convection stagnation point flows of an electrically conducting Maxwell fluid. Joule heating, non-linear radiation, thermal conductivity and convective heat transfer are considered. Finite difference scheme is applied to get the solutions. Non-linear Rosseland approximation is used for radiative heat transfer of two viscoelastic fluids by Cortell [19]. Das *et al.* [20] discussed the non-linear radiative heat flux in flow of Jaffery fluid over a stretching sheet. They utilized the Runge-Kutta-Fehlberg scheme to compute the solutions.

The aforementioned studies depict that heat transfer through non-linear thermal radiation is not much examined. Marangoni flows are also less attended for realistic fluids because of the highly non-linear boundary conditions. Flows by an inclined channel with different inclination of magnetic field is also not discussed. Motivated by these facts, we study the Marangoni convective flow of an electrically conducting Carreau fluid over a porous inclined surface. Non-linear thermal radiation, thermal conductivity, Joule heating and viscous dissipation effects are accounted. Runge-Kutta-Fehlberg scheme [21-24] is utilized to compute the numerical solutions. The article is structured as follows. First section contributed toward the brief introduction of study. In second section, mathematical problem is formulated and non-dimensionalized. Third section comprises the numerical procedure. Analysis and comparison of study with Hayat *et al.* [25] are given in fourth section whereas conclusions are presented in section five. References are listed in the sixth section.

Problem statement

In this paper the steady Marangoni convection flow driven by a temperature gradient in electrically-conducting Carreau liquid is considered. The 2-D analysis is presented by an inclined surface [5]. Effects of MHD, buoyancy and external pressure gradient are considered. Permeable surface subject to suction/injection is taken. Analysis of heat transfer is carried out through viscous dissipation, Joule heating and thermal radiation. Thermal stratification is also considered. The governing equations of this study are based on the balance laws of mass, momentum and energy. Taking the previous assumptions into consideration, the boundary-layer equations can be written in dimensional form:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0 \tag{1}$$

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} = -\frac{\Delta B_0^2}{\rho}u\sin^2\psi + v\left[1 + \lambda^2\left(\frac{n-1}{2}\right)\left(\frac{\partial u}{\partial y}\right)^2\right]\frac{\partial^2 u}{\partial y^2} + v(n-1)\lambda^2\left[1 + \lambda^2\frac{3}{4}\left(\frac{n-3}{2}\right)\left(\frac{\partial u}{\partial y}\right)^2\right]\frac{\partial^2 u}{\partial y^2}\left(\frac{\partial u}{\partial y}\right)^2 + g\beta\sin\phi(T - T_{\infty})$$
(2)

$$\rho c_{p} \left(u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} \right) = k \frac{\partial^{2} T}{\partial y^{2}} - \frac{\partial q_{r}}{\partial y} + \Delta B_{0}^{2} u^{2} \sin^{2} \psi + \eta_{0} \left[1 + \lambda^{2} \left(\frac{n-1}{2} \right) \left(\frac{\partial u}{\partial y} \right)^{2} + \lambda^{4} \frac{1}{2} \left(\frac{n-1}{2} \right) \left(\frac{n-3}{2} \right) \left(\frac{\partial u}{\partial y} \right)^{4} \right] \left(\frac{\partial u}{\partial y} \right)^{2}$$
(3)

where u and v are the x and y components of velocity, respectively, η_0 – the dynamic viscosity, Δ – the electric conductivity, B_0 – the uniform magnetic field strength, ρ – the density of fluid, n – the power index, λ – the time constant, β – the thermal expansion coefficient, c_p – the specific heat at constant pressure, T – the fluid, $T_s(x)$ – the temperature interface, T_{∞} – the fluid temperature far from the surface, k – the thermal conductivity of fluid, q_r – the radiative heat flux, ψ – the angle of magnetic field, ϕ – the inclination angle of surface, and v – the kinematic viscosity. The non-linear form of thermal radiation:

$$q_r = -\frac{4\delta^*}{3k^*}\frac{\partial T^4}{\partial y} = -\frac{16\delta^*}{3k^*}T^3\frac{\partial T}{\partial y}, \quad \frac{\partial q_r}{\partial y} = -\frac{16\delta^*}{k^*}T^2\left(\frac{\partial T}{\partial y}\right)^2 - \frac{16\delta^*}{3k^*}T^3\frac{\partial^2 T}{\partial y^2} \tag{4}$$

in which δ^* is the Stefan-Boltzmann constant and k^* the mean absorption coefficient. The corresponding boundary conditions:

$$\eta_0 \left[1 + \lambda^2 \left(\frac{n-1}{2} \right) \left(\frac{\partial u}{\partial y} \right)^2 + \lambda^4 \frac{1}{2} \left(\frac{n-1}{2} \right) \left(\frac{n-3}{2} \right) \left(\frac{\partial u}{\partial y} \right)^4 \right] \left(\frac{\partial u}{\partial y} \right) = -\frac{\mathrm{d}\delta}{\mathrm{d}T} \frac{\mathrm{d}T}{\mathrm{d}x}$$
(5)
$$v(x, y) = v_w, \quad T(x, y) = T_s = Ax^2 + T_0, \text{ at } y = 0$$
$$u \to 0, \quad T \to T_\infty = Bx^2 + T_0, \text{ when } y \to \infty$$
(6)

where v_w is constant mass transfer velocity with $v_w < 0$ for suction and $v_w > 0$ for injection, A and B – the temperature gradient coefficients, and δ – the surface tension:

$$\eta = c_1 y, \quad \Psi(x, y) = \frac{x}{c_2} f(\eta), \quad u = \frac{\partial \Psi}{\partial y}, \quad v = -\frac{\partial \Psi}{\partial x}$$

$$c_1 = \sqrt[3]{\frac{\rho A\left(\frac{d\delta}{dT}\right)}{\mu^2}}, \quad c_2 = \sqrt[3]{\frac{\rho^2}{\mu A\left(\frac{d\delta}{dT}\right)}}, \quad \theta = \frac{T - T_{\infty}}{T_s - T_0}$$
(7)

Equation (1) is trivially verified whereas the dimensionless boundary-layer problems:

$$f'^{2} - ff'' = f''' \left[1 + \frac{n-1}{2} \lambda_{1} f''^{2} \right] + \lambda_{1} f''' f''^{2} (n-1) \left[1 + \frac{3}{4} \left(\frac{n-3}{2} \right) \lambda_{1} f''^{2} \right] + \beta^{*} \sin \phi \theta - M^{2} \sin^{2} \psi f'$$
(8)

$$\theta'' + 4R(\theta_r - \theta_s) \Big[1 + (\theta_r - \theta_s) \theta \Big]^2 \theta'^2 + \frac{4}{3} R \Big[1 + (\theta_r - \theta_s) \theta \Big]^3 \theta'' + + \Pr \operatorname{Ec} \Big[1 + \Big(\frac{n-1}{2} \Big) \lambda_1 f''^2 + \frac{1}{2} \Big(\frac{n-1}{2} \Big) \Big(\frac{n-3}{2} \Big) \lambda_1^2 f''^4 \Big] f''^2 - - \Pr \Big[2S_t f' + 2f' \theta' - f \theta' \Big] + M^2 \operatorname{Pr} \operatorname{Ec} \sin^2 \psi f'^2 = 0$$
(9)

$$\left[1 + \left(\frac{n-1}{2}\right)\lambda_1 f''^2 + \frac{1}{2}\left(\frac{n-1}{2}\right)\left(\frac{n-3}{2}\right)\lambda_1^2 f''^4\right]f'' = -2$$
(10)

$$\begin{aligned} f &= \alpha, \ \theta = 1 - S_t, \ \text{at} \ \eta = 0 \\ f' &\to 0, \ \theta \to 0, \ \text{when} \ \eta \to \infty \end{aligned}$$
(11)

In previous equations:

$$\lambda_{1} = \frac{\lambda^{2} c_{1}^{4} x^{2}}{c_{2}^{2}}, \quad \beta^{*} = \frac{g\beta Ax c_{2}^{2}}{c_{1}^{2}}, \quad M^{2} = \frac{\Delta B_{0}^{2} c_{2}}{\rho c_{1}}, \quad Ec = \frac{c_{1}^{2}}{A c_{p} c_{2}^{2}},$$

$$R = \frac{4\delta^{*} T_{\infty}^{3}}{k^{*} k}, \quad Pr = \frac{\eta_{0} c_{p}}{k}, \quad S_{t} = \frac{B}{A}, \quad \theta_{r} = \frac{T_{s}}{T_{\infty}}, \quad \theta_{s} = \frac{T_{0}}{T_{\infty}}, \quad \alpha = -c_{2} v_{w}$$
(12)

where $f(\eta)$ is the dimensionless velocity, $\theta(\eta)$ – the dimensionless temperature, R – the radiation parameter, Pr – the Prandtl number, M – the Hartmann number, λ_1 – the fluid constant, Ec – the Eckert number, θ_r , θ_s – the temperature constants, β^* – the mixed convection parameter, S_t – the stratification parameter and α – the porosity constant. Local Nusselt number:

$$Nu = \frac{q_w x}{k(T_s - T_0)}, \quad q_w = -\left(k\frac{\partial T}{\partial y} + \frac{16\delta^*}{3k^*}T^3\frac{\partial T}{\partial y}\right)_{y=0}$$
(13)

Non-linear Nusselt number:

$$\operatorname{Re}_{x}^{-1/2}\operatorname{Nu} = -\left\{1 + \frac{4}{3}R[1 + (\theta_{r} - \theta_{s})\theta(0)]^{3}\right\}\theta'(0), \text{ with } \operatorname{Re}_{x} = c_{1}^{2}x^{2}$$
(14)

Numerical procedure

In this study, the non-linear eqs. (8)-(9) with highly non-linear boundary conditions (10) are successfully solved by implementing an efficient numerical scheme Runge-Kutta-Fehlberg fourth fifth (RKF-45) order. Marangoni convection flow is discussed numerically. The effects of pertinent parameters are scrutinized for the dimensionless velocity, temperature and the rate of heat transfer. The step size and convergence criteria are chosen to be 0.001 and 10⁻⁶, respectively. Asymptotic boundary conditions in eq. (10) are approximated by using a value of 10:

$$\eta_{\max} = 10, \quad f'(10) = \theta(10) = 0$$
 (15)

This ensures that all numerical solutions approached the asymptotic values correctly.

Analysis

This section comprises analysis of numerical results for the velocity and temperature profiles of an electrically conducting Carreau fluid due to porous inclined surface. Effectiveness of involved physical parameters is discussed through graphs and tables for the non-linear thermal radiative heat transfer, applied magnetic field, inclination of applied magnetic field, mixed convection, porosity of inclined surface, thermal stratification, power index of Carreau fluid, inclination of surface, heat dissipation, convection-conduction characteristics and momentum-thermal diffusivity. Figures 1-5 describe the dimensionless velocity, $f'(\eta)$, situations for the changing aspects of physical properties through assigning the particular values to involved parameters. Figures 6-10 give thermal behavior of current flow situations by dimensionless temperature distributions, $\theta(\eta)$, and fig. 11 defines the varying heat flux through Nusselt number. Table 1 is presented to see the parametric effects on numerical values of Nusselt number. Table 2 is expanded to compare the numerical values of -f''(0) with Hayat *et al.* [25] for different values of Hartmann number.

The involved physical parameters are the radiation parameter, R, fluid constant, λ_1 , Hartmann number, inclination of applied magnetic field, ψ , mixed convection parameter, β^* , porosity of inclined surface, α , thermal stratification parameter, S_i , power index, n, inclination of surface, ϕ , Eckert number, temperature constants, θ_r and θ_s , Nusselt and Prandtl numbers.



Figure 1. Effects of Hartman number, and fluid constant, λ_1 , on $f'(\eta)$



Figure 3, Effects of porosity constant, α , and surface inclination, ϕ , on $f'(\eta)$



Figure 5. Effects of radiation parameter, R, and Eckert number, on $f'(\eta)$



Figure 2. Effects of mixed convection parameter, β^* , and power index, *n*, on $f'(\eta)$



Figure 4. Effects of thermal stratification, S_t , and inclination of magnetic field, ψ , on $f'(\eta)$



Figure 6. Effects of Hartman number, and radiation parameter, R, on $\theta(\eta)$



Figure 7. Effects of Eckert number, and power index, *n*, on $\theta(\eta)$



Figure 9. Effects of fluid constant, λ_1 , and surface inclination, ϕ , on $\theta(\eta)$



Figure 8. Effects of thermal stratification, S_i , and mixed convection, β^* , on $\theta(\eta)$



Figure 10. Effects of interface temperature, θ_r , and reference temperature, θ_s , on $\theta(\eta)$

Figure 1 is sketched for the behavior of dimensionless velocity $f'(\eta)$ when two important physical parameters the fluid constant, λ_1 , and the Hartmann number increase. Enhancement of both fluid constant and Hartmann number decelerates the fluid velocity $f'(\eta)$. In this peculiar flow situation, the enhancement of fluid constant is directly proportional to Marangoni number, c_1 . Direct increase in λ_1 uplifts the surface tension rate with high density that eventually decelerates the fluid velocity. The accelerating behavior of velocity $f'(\eta)$ for the expansion of mixed convection parameter, β^* , and power index, n, is detected in fig. 2. The response of power index, n, is recorded for its two values *i. e.*, n = 1 and n = 3. Obviously for n = 3, fluid velocity $f'(\eta)$ has higher value than n = 1. Figure 3 reported the upshots of porosity parameter, α , and inclination of surface, ϕ , on fluid velocity $f'(\eta)$ significantly reduced. This situation occurs owing to the larger suction rate at $\alpha = 1.5$. An interesting observation for enhancement in fluid velocity $f'(\eta)$ is also observed in fig. 3 via making the surface more inclined through increasing ϕ . Large values of inclination of applied magnetic field, ψ , and thermal stratification

parameter, S_t , decay the fluid velocity $f'(\eta)$, see fig. 4. The applied magnetic field has greater decelerating impact on velocity when applied at $\psi = 0$ and this effect decreases for higher values of inclination angle (for $\psi = \pi/4$ and $\psi = \pi/2$). Similar behavior of velocity is noted for thermal stratification parameter, S_{t} , in this figure. Figure 5 is displayed for impact of radiation parameter, R, and Eckert number on fluid velocity $f'(\eta)$. The intense radiations (by changing R from 0 to 5) provides the high kinetic energy for fluid-flow that in turns accelerates fluid motion, by increasing $f'(\eta)$. Eckert number (which is the heat dissipation factor) also has an accelerating effect, see fig. 5. Impact of varying radiation parameter, R, and Hartmann number on temperature profile $\theta(\eta)$ has been displayed in fig. 6. Two cases of magnetic field impact on temperature are discussed for increasing radiation parameter. Solid line gives the heated radiation effects in the absence of magnetic field, M = 0, (and dashes depicts the same thermal fluid nature in the presence of magnetic field, M = 1. Clearly temperature $\theta(\eta)$ is increased for later case. The heated nature of Eckert number and power index, n, is explained through fig. 7. Figure 8 is presented to examine the influence of mixed convection parameter, β^* , and stratification parameter, S_t , on temperature distribution $\theta(\eta)$. This figure depicts that for larger β^* and thermal stratification, S_t , the fluid's temperature $\theta(\eta)$ decays. In fig. 9, the impact of inclination angle, ϕ , on temperature profile $\theta(\eta)$ is studied for two cases of fluid constant, λ_1 . Here solid line describes viscous fluid case with $\lambda_1 = 0$ and dashes depict the Carreau liquid-flow situations with $\lambda_1 = 1$. In both situations, temperature profile $\theta(\eta)$ decreased but the fluid is more heated in case of Carreau liquid when compared with viscous fluid situation. Significant impacts of two constants, θ_r and θ_s , on temperature $\theta(\eta)$ are given through fig. 10. Both the temperature constants, θ_r and θ_s , have tendency to cool down the fluid but the interface temperature constant θ_r rapidly lowers the temperature when compared to θ_s . Nusselt number is discussed in fig. 11 for radiation parameter, R, fluid constant, λ_1 , Eckert number, and thermal stratification parameter, S_t. Figure 11(a) indicates that the fluid constant, λ_1 , and radiation parameter, R, enhance the Nusselt number whereas fig. 11(b) shows that Eckert number and thermal stratification, S₀, have reverse effects on Nusselt number. Numerical treatment Nusselt number for current situation is given in tab. 1. Numerical values of Nusselt number reveal that larger values of Hartmann number, inclination of surface, ϕ , inclination of magnetic field, ψ , and Eckert number, the Nusselt number decays. On the other hand the Nusselt number enhances for larger values of fluid constant, λ_1 , porosity parameter, α , radiation parameter, R, and thermal stratification parameter, S_t. Comparison for the numerical



Figure 11. Parametric effects on Nusselt number

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values of -f''(0) is given in tab. 2. It is observed in this table that the present results matches exactly with the existing literature [25] for $0 \le M \le l$ and matches upto 4th decimal place for values $M \ge 1$.

parameter		-,	_, .,,	• 3 • • • • • • •				
М	λ_1	α	R	S_t	ϕ	Ψ	Ec	$\operatorname{Re}_{x}^{-1/2}\operatorname{Nu}$
0	0.2	0.1	0.2	0.1	π/3	π/4	0.2	0.159728
0.2								0.158108
0.5								0.150117
1.0	0.1							0.142718
	0.3							0.172499
	0.5							0.186896
	0.2	0.2						0.191871
		0.3						0.228077
		0.4						0.268083
		0.1	0.0					0.085701
			0.5					0.260525
			1.0					0.404323
			0.2	0.0				0.069075
				0.3				0.328429
				0.5				0.483021
				0.1	π/6			0.159887
					π/4			0.159602
					π/3			0.159321
					π/3	π/6		0.159524
						π/4		0.159320
						π/3		0.159117
						π/3	0.0	0.332896
							0.1	0.245944
							0.3	0.072412

Table 1. Numerical values of Nusselt number for different physical parameters when Pr = 1, n = 0.2, $\theta_r = 0.4$, $\theta_s = 0.3$, and $\beta^* = 0.2$

Table 2. Comparison of -f''(0) with Hayat *et al.* [25] for different values of Hartmann number when $\lambda_1 = 0$, n = 1, $\alpha = 0$, $\beta^* = 0$, $\phi = 0$, $\psi = 90$

	- <i>f</i> "(0)				
М	[25]	RKF-45 (Present)			
0.0	1.00000	1.00000			
0.2	1.01980	1.01980			
0.5	1.11803	1.11803			
0.8	1.28063	1.28063			
1.0	1.41421	1.41422			
1.2	1.56205	1.56207			
1.5	1.80303	1.80306			

Conclusions

Numerical treatment is presented for the examination of Marangoni convective flow of magneto Carreau fluid over a permeable inclined surface with convective boundary conditions. The salient features are mentioned below.

- The inclination of surface and thermal stratification dampens the fluid motion and the heat transfer processes.
- Presence of Carreau fluid slows down the velocity but heats up the fluid.
- Non-linear radiation behaves as regulating the fluid motion, Nusselt number and heat transfer processes.
- Fluid motion and heat transfer have reverse behavior for mixed convection parameter, Hartmann number and power index.
- Thermal field shows opposite response for the reference and interface temperatures.

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