

PERFORMANCE CHARACTERISTICS OF MECHANICAL DRAFT COOLING TOWERS IN THERMAL POWER PLANT

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Generated power of thermal power plant is closely related to efficient work of cooling towers, via condenser pressure affected by output temperature of cooling water. Performance characteristics of cooling system can be rated via several parameters such as: thermal effectiveness, Merkel number, Number of Transfer Units and overall heat and mass transfer coefficient. Results gathered during acceptance test of cooling system of Thermal power plant Kakanj (unit 7) which consists of 12 wet counterflow induced draft cooling towers, are used to evaluate its most important performance characteristics. It is shown that some tower performance characteristic vary during the day more than others due to their dependence on climatic parameters, particularly air wet bulb temperature. Different approaches and methods (analytical and empirical) for evaluation of tower performance are discussed in order to define the most appropriate performance characteristic and calculation method which can be used for establishing the optimal working mode of analysed cooling system.

Key words: cooling tower, performance characteristics, climate parameters, optimal operation mode

1. Introduction

Cooling tower is a type of heat exchanger often used to dissipate heat in Clausius-Rankine cycle and it serves as so called "cold end" of thermal power plant (TPP) system. Turbine exhaust steam condenses in a condenser while heat is removed via cooling water as heat transfer medium, which circulates through the condenser tubes. Heated water from the condenser's tubes is afterwards pumped to the cooling tower, where, in case of commonly used wet cooling towers, it is cooled by simultaneous heat and mass transfer to the ambience air. Re-cooled water then returns to the condenser for new cycle. In the system of counterflow cooling towers, simultaneous heat and mass transfer takes place while cooling water flows downwards over the tower film-type fill and it is exposed to the atmospheric air that flows upwards. During the process, water temperature decreases while air temperature and humidity increases. Figure 1 provides schematic view of cold end system and its connection to the steam turbine.

Theoretically, tower output water temperature can be lowered near to the air wet bulb temperature which indicates that the process is in great manner affected by the environmental climate conditions. On the other hand, temperature of the circulating water at the outlet of cooling tower is of the great importance since it directly affects the condenser pressure of turbine exhaust steam in the condenser.

Further on, the condenser pressure determines the enthalpy drop of steam in the low-pressure turbine and finally it conditions the generated power. This implicates that lower tower output water temperature can increase generated power in turbine and that the efficiency of the turbine cycle is conditioned, among other factors, by climate parameters of its environment through operation of cooling towers. Following this logic, correlation between the generated power in low pressure turbine and climate conditions of environment is derived and presented in [1]

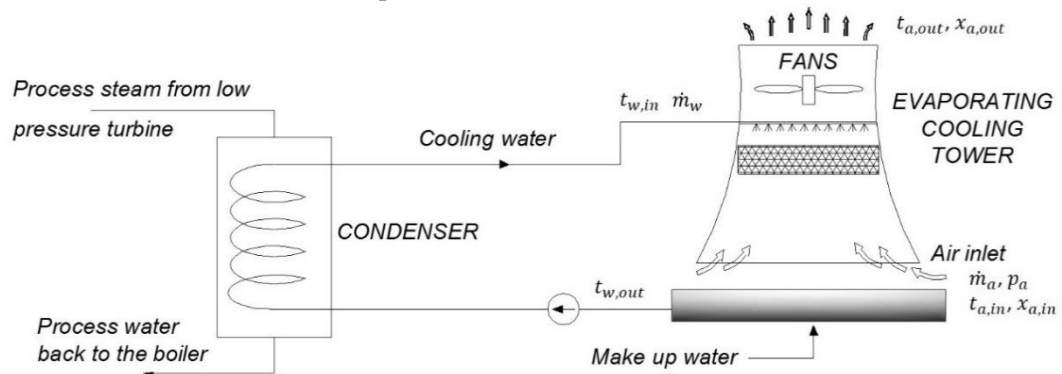


Fig. 1. Schematic view of TPP's cold end connected to the low-pressure turbine

In the design phase, thermal capability of cooling towers is determined by water volumetric flow rates, water inlet and outlet temperatures (cooling tower range) and inlet air wet bulb temperature (therefore cooling tower approach). In this phase, it is common to use adequate software for design purpose, but empirical and experimental data can also be of great value depending on design conditions [2]. Counterflow wet cooling tower theory is explained in detail in [2], [3] and [4], where various cooling towers performance characteristics are defined and its mathematical and empirical correlations are derived. In practice, Merkel method or Poppe's method are most commonly used for calculating some tower performance characteristics such as Merkel number, mass transfer coefficient and also Number of Transfer Units. Other commonly used parameters for evaluation of thermal performance characteristics are tower effectiveness, cooling tower range (range) and cooling tower approach (approach). All of the parameters are affected by the parameters of ambience air, particularly air wet bulb temperature, however daily and seasonal variations of climate parameters are not considered during the design phase. Therefore, it is of great importance to ensure that performance characteristics are kept in nominated range during the operation period to prevent decrease of generated power of TPP resulting from increased tower outlet water temperature. In the light of this intention, determination of most suitable performance characteristics would enable implementation of targeted optimisation and correction of day-to-day and seasonal operation mode. The chosen performance characteristics need to be sensitive to changes of climatic parameters and they should clearly indicate which input parameters could improve current operation of cooling towers system.

In this paper, evaluation of several performance characteristics is presented, based on results of measurements taken during the acceptance testing for cooling towers of Unit 7 in Thermal Power Plant "Kakanj", near the city of Kakanj in Bosnia and Herzegovina. The performance characteristics are computed using different approaches, mathematical expressions and empirical correlations in order to examine which characteristics are most suitable to describe the towers performance in regards to variations of climate parameters. Overall intention of this analysis is to contribute to development of dynamic process of optimisation during the operation mode.

2. Measurement data

The cooling towers in TPP Kakanj (Unit 7) are wet, counterflow induced draft with air flow ensured with fans of 160 kW individual power. Cooling water flow is enabled with circulating pump and it is distributed between operating towers via valve with electromotor drive. After entering the cooling tower, the water is distributed through spray type distributors (nozzles) and to the film type packing made from plastic. Design parameters are defined as follows: 10 cooling towers for exploitation and additional 2 towers as backup, water volumetric flow rate 24490 m³/h, inlet water temperature is 38.7°C and the outlet water temperature is 27.0 °C for air wet bulb temperature 22°C.

Acceptance testing of cooling towers was performed in line with DIN 1947. During the testing, 10 out of 12 towers were in operation. Testing includes measurements of parameters during the period of 24 hours in summer time. Most important measured values are shown in Table 1.

Table 1. List and ranges of most important measured parameters during acceptance testing

Measured parameters	Unit	Range of values	Average values
Air dry bulb temperature at the tower inlet, $t_{a,in}$	°C	14.6 – 30.3	-
Air wet bulb temperature at the tower inlet, $t_{awb,in}$	°C	14.1 – 22.9	-
Water inlet temperature, $t_{w,in}$	°C	34.4 – 38.9	36.68
Water outlet temperature, $t_{w,out}$	°C	23.1 – 27.5	25.51
Water mass flow rate at the tower inlet, \dot{m}_w	kg/s	6452.0 -6954.4	6498.8

It is evident that the parameters during the testing period were in expected ranges of values and not exceeding design conditions, but the summer period can easily create unfavourable conditions for tower operation. With the increase of dry bulb temperature, sensible heat flow can even change its direction and the ambient air will start heating the water. On the other hand, the web bulb temperature in mild continental climate such as in location of Kakanj, will always provide potential for evaporative cooling and will keep the overall heat flow in direction from water to the air. This situation is considered very rare, appearing during 0,1-0,2% of tower operation time [5] and in case of thermal power plant it will not endanger the electricity generation process itself but only decrease generated power for short period.

3. Calculation model for heat transfer rates and discussion of results

Total heat rate exchanged in the cooling tower, Q_{CT} (kW), is calculated using overall energy balance of water:

$$Q_{CT} = \dot{m}_w(i_{w,in} - i_{w,out}) \quad (1)$$

Total heat rate is equal to the energy that the air stream takes over which results in the air enthalpy change. Also, energy balance for air enables another representation of heat transfer rate that consists of two components – sensible and evaporative heat, [5] as:

$$\begin{aligned} Q_{CT} &= \dot{m}_a(i_{a,out} - i_{a,in}) = Q_{a,lat} + Q_{a,sens} \\ &= \dot{m}_a(x_{a,out} - x_{a,in})i_{fg} + \dot{m}_a c_{p,a}(t_{a,out} - t_{a,in}) \end{aligned} \quad (2)$$

where i_{fg} (Jkg^{-1}) is latent heat of vaporization. It is visible that the latent heat rate is driven by change of humidity ratio of dry air, while sensible heat transfer rate is driven by change of air dry bulb temperature. The humidity ratio (mass ratio of water vapor to dry air) x_a ($\text{kg}_w\text{kg}_a^{-1}$) is calculated as [2]:

$$x_a = 0,622 \frac{\varphi p_{sat}}{p_a - \varphi p_{sat}} \quad (3)$$

where p_{sat} is saturation pressure for current dry bulb air temperature. Enthalpy of the moisture-air mixture in (kJkg^{-1}) is calculated as [2]:

$$i_a = (0.24t_a + x_a(595 + 0.46 \cdot t_a)) \cdot 4186.8 \quad (4)$$

Calculation procedure was as follows: using the eq. (1) total heat transfer rate is calculated. Relative humidity of air at inlet of cooling tower is determined using the values of measured meteorological data at the location of power plant which include ambient air temperature, ambient air pressure and wet bulb temperature, and results are given in Figure 2. Air flow rate is determined using the fan performance curve. From the total heat transfer rate and eq. (2), outlet air enthalpy is calculated. Using the Mollier diagram, dry bulb air outlet temperature is determined using enthalpy and assumption that air is at saturated state. Sensitive and latent heat transfer rates are calculated using the equation (2).

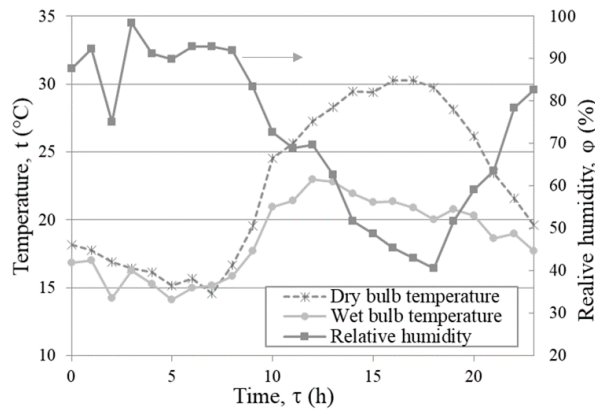


Fig. 2. Ambient air parameters at the location of TPP Kakanj

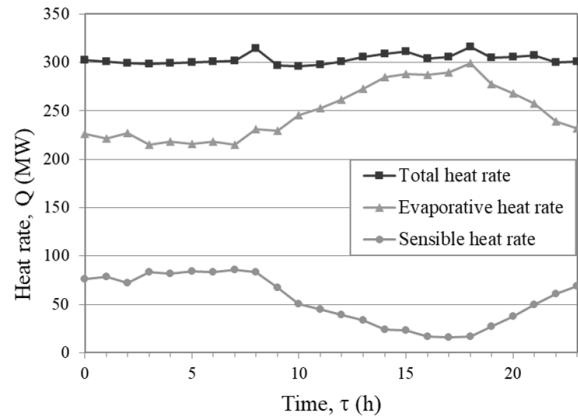


Fig. 3. Heat rates transferred during the 24h period in TPP Kakanj cooling towers

From Figure 2. it is evident how much the climatic parameters of air vary only within one full day, as well as particular heat rates are shown in Figure 3. It is visible that evaporative heat rate is dominant over the sensible heat rate, ranging from 71 % to 94 % in total heat rates exchange. These results show that the total heat rate is mainly controlled by the evaporative (latent) heat rate which is in line with results presented in [5]. However, the relation between the evaporative heat rate and the climate conditions of environment are not as straight forward as in case of sensible heat rate which can easily be related to dry bulb air temperature, as shown in Fig 2 and 3.

In order to explain more clearly the dependence of evaporative heat rate from ambient conditions, the climate parameters of air entering and exiting the tower are shown in Mollier's i - x . As noticeable in Figure 4, dots on left hand side represent the conditions of inlet air at the entrance of tower and the triangles on right hand side show the state of air at the exit of the tower. For analysing and predicting the

evaporative heat rate tendency, most important parameter is the potential of air for receiving the moisture from the cooling water within the tower. This potential is a difference of humidity ratio of air between tower exit and entrance, Δx . For bigger relative humidity difference Δx , the ambient air can receive more moisture and the evaporative heat rate in the tower is higher. If the results from figures 2, 3 and 4 are compared, it can easily be noticed that the lowest relative humidity and highest dry bulb temperature are around 18h (Fig 2) which enables highest increase of humidity ratio (Δx_{max}) and the highest evaporative heat rate (Fig 3). Lowest potential for evaporative heat rate is found to be around 3 h, when the dry bulb temperature is low and the relative humidity is highest.

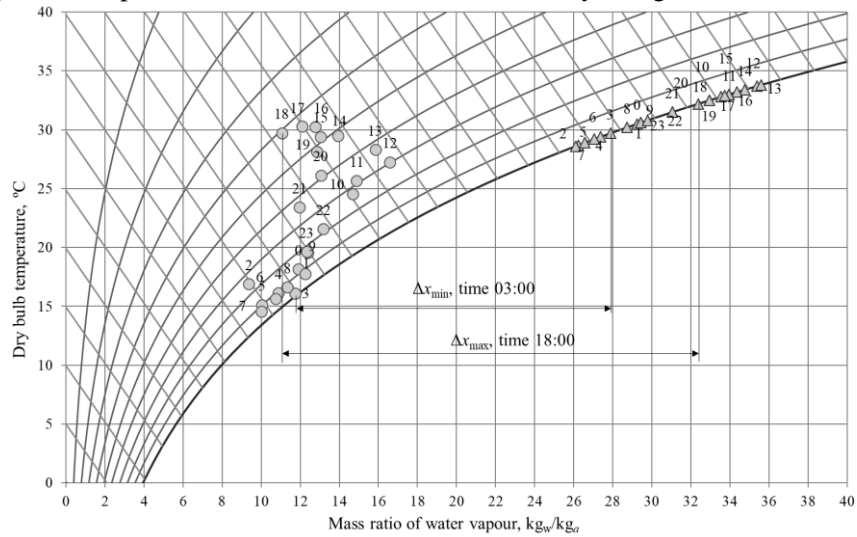


Fig. 4. Mollier diagram of moist air with air states at inlet (dot) and outlet (triangle) of tower

For validation, values of calculated evaporated water mass flow rate are compared with measured values of makeup water mass. The makeup water needs to cover three types of water losses from the cooling tower: 1) evaporation loss, 2) drift loss and 3) slug loss. Water loss due to its evaporation in cooling towers is dominant and continuously present. If the air at outlet of tower is supersaturated, it contains water droplets which represent drift loss. Finally, due to the constant loss of clear water through evaporation, the density of water flowing through towers increases and a certain amount of water needs to be replaced by fresh makeup water. This is done periodically by discharging some water from cooling tower basin. During the performed acceptance testing of cooling towers, there was no discharge of water from the basin. Therefore, the slug loss was not taken into consideration for validation of results based on mentioned measurements.

Evaporated water is calculated as:

$$\dot{m}_{evap} = \dot{m}_a(x_{a,out} - x_{a,in}) \quad (5)$$

Values of calculated evaporated water and measured make up water mass differ around 4 % in average, which is satisfactory since makeup water covers also drift losses. Air velocity expressed for fill cross flow area was $3,09 \text{ ms}^{-1}$, which is smaller than limited values of $3,5 \text{ ms}^{-1}$ therefore upward transfer of water through the fill and resulting drift losses are minimized [4] and kept under guaranteed values smaller than 2 %. Moreover, the makeup water control system is rather sluggish in its response to tower water losses and it also creates deviation in comparison of values between the two water mass flow rates.

4. Performance characteristics of examined cooling towers

In this chapter, several characteristic parameters for evaluation of cooling tower performance have been calculated on the basis of data collected at examined cooling towers system in TPP Kakanj. The results have been discussed with the aim to find parameters which could be useful for managing the tower system operation in most effective way.

4.1. Thermal effectiveness, Cooling range and Approach

Thermal effectiveness of cooling tower is expressed as a ratio of cooling range and sum of cooling range and approach. It can also be represented as actual temperature difference of cooling water as it flows through the cooling tower and a maximum theoretical temperature difference [6] and [7]:

$$\varepsilon = \frac{Range}{Range + Approach} = \frac{t_{w,in} - t_{w,out}}{t_{w,in} - t_{awb,in}} \quad (6)$$

Cooling range of cooling tower is defined as difference between water inlet and outlet: $Range = (t_{w,in} - t_{w,out})$ and approach as difference: $Approach = (t_{w,out} - t_{awb,in})$. In tower operation both values must be greater than zero, while smaller value of approach represents better cooling tower operation and consequently it can improve the efficiency of the TPP system. However, there is a limitation for this parameter on the side of condenser. Namely, the exhaust steam from low pressure turbine needs to be fully transformed to liquid state in condenser (see Fig 1) but it must not be cooled too much below the condensation temperature. If the climate conditions of environment are suitable for high cooling performance of towers, like in winter time, there is a risk for subcooling the condensate which will then require more heat energy in boiler during the next cycle. Therefore, thermal effectiveness should be improved but under the condition to keep the outlet water temperature at the desired value.

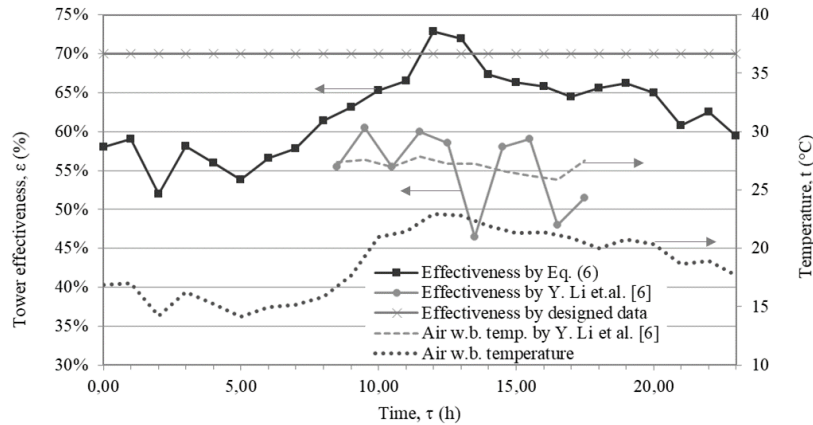


Fig. 5. Tower effectiveness and inlet air wet bulb temperature

Thermal effectiveness is a function of inlet air wet bulb temperature and it increases while inlet air temperature increases. This is shown on tested cooling tower and it is visible in Fig. 5 by comparing the values of tower thermal effectiveness and values of air wet bulb temperature. Based on design inlet values for cooling towers in TPP (Unit 7), value of thermal effectiveness is 0.7 (that is 70 %), while range is 11.7 °C and approach is 5 °C. Also, it is clear from eq. (6) that tower approach plays important

role and that while tower outlet water temperature gets closer to the air wet bulb temperature (therefore air humidity increases) effectiveness of tower increases. In usual operation mode, approach has a value approximately 5 – 6 °C [8] or even smaller [9]. Effectiveness of tested tower was in the range from 52 to 72 %, which shows a great dependence of outlet air properties and it also indicates lack of control system sensitive to variations of climate parameters of environment. Results from [6] show lower tower effectiveness values than examined towers in Kakanj, as a result of smaller air wet bulb temperature.

Another formulation of tower effectiveness is given in [10] as:

$$\varepsilon^* = \frac{\varepsilon}{1 - \varepsilon} = \frac{t_{w,in} - t_{w,out}}{t_{w,out} - t_{awb,in}} \quad (7)$$

Values of ε^* are calculated for conditions in TPP Kakanj which correspond to the ones presented in [10], Case 4. Corresponding measurements are taken in 10 h: inlet water temperature 36,6 °C, outlet water temperature 26.4 °C and ambient air wet bulb temperature 20.9 °C. Calculated thermal effectiveness is 1.88 which show good compatibility with results of Mansour (case 4; thermal effectiveness 1.62), which means that this method could be implemented for examining the effectiveness of TPP Kakanj cooling tower. However, thermal effectiveness calculated as given in eq. (7) is rather developed to be used in relation with other important tower performance characteristic (Number of Transfer Units) and this will be further investigated in following chapters.

It is shown that effectiveness of cooling of the water film depends on the ratio of water to air mass flow rates and decreases while ratio increase [7]. During the measurement, ratio of mass flow rates was preserved in approximately constant values around 1.064, so this effect was not tested. However, the control of cooling system in towers can be done most easily through modification of air mass flow rate. Therefore, investigation of this dependence would be of great value for the process of optimisation.

4.2. Merkel's number

In practice, most frequently used theory for performance evaluation of cooling towers is Merkel method, which enables calculation of several performance characteristics: Merkel number, overall heat and mass transfer or Number of transfer units.

The Merkel number by Merkel's methods is presented in the following equation as [2]:

$$Me = \frac{h_d \cdot A}{\dot{m}_w} = \frac{h_d \cdot a_{fi} \cdot L_{fi}}{\dot{G}_w} \left(= \frac{K \cdot a \cdot V}{L} \right) \quad (8)$$

where, h_d or K ($\text{kgm}^{-2}\text{s}^{-1}$) is mass transfer coefficient, A (m^2) is the heat and mass transfer surface area, a_{fi} or a (m^2m^{-3}) is transfer surface area per unit volume V , \dot{G}_w ($\text{kgm}^{-2}\text{s}^{-1}$) is mass velocity expressed as a ratio of water mass flow rate and fill cross flow area, L_{fi} (m) is fill height and \dot{m}_w or L (kgs^{-1}) is the water mass flow rate. Most important assumptions of the model are that Lewis factor is equal to unity, air at the output of the cooling tower is saturated, air at the inlet of tower fill is of the same parameters as the air at the inlet of tower (ambient conditions) and evaporated water mass flow rate is neglected in the energy balance. For known values of water and air temperatures at the inlet and outlet, Merkel number

could be calculated using following equation (shown also as an algebraic equation, using the four-point Chebyshev integration technique [11]):

$$Me = \int_{t_{w,in}}^{t_{w,out}} \frac{c_{pw} \cdot dt_w}{i_{a,sat} - i_a} = 0.25 \cdot c_{pw} \cdot (t_{w,in} - t_{w,out}) \sum_{j=1}^4 \frac{1}{(i_{a,sat} - i_a)_j} \quad (9)$$

where, $i_{a,sat}$ (kJkg⁻¹) is enthalpy of saturated air calculated for the water temperature of adjacent film of water and i_a (kJkg⁻¹) is enthalpy of bulk moisture-air mixture.

Empirical relation for the Merkel number is given as a function of mass velocities of air and water and inlet film temperature in [4] as:

$$\frac{Me}{L_{fi}} = 4.299 \frac{\dot{G}_a^{0.711}}{\dot{G}_w^{0.657} t_{w,in}^{0.476}} \quad (10)$$

Another empirical relation for Merkel number is given in [12] and it connects values of Merkel number and ratio of air to water mass flow rates using empirical coefficients. The coefficients m and n are related to the condition of tower packing, i.e. their values decrease when the packing is damaged or fouled. For newly designed or reconstructed cooling towers the coefficients with values of $m=1.82$ and $n=0.61$ are given and they fit to the conditions of acceptance testing. The relation from [12] then becomes:

$$Me = m \left(\frac{\dot{G}_a}{\dot{G}_w} \right)^n = 1.82 \left(\frac{\dot{G}_a}{\dot{G}_w} \right)^{0.61} \quad (11)$$

Values of Merkel number are calculated for 24-hour period using the eq. 9, 10 and 11. The results are shown in Fig. 6 and it is visible that the values according to Merkel equations vary in time as a function of outlet air parameters change while empirical equations give approximately uniform values of Merkel number. This can be easily explained by taking into consideration the fact that the water and air mass flow rates, which are main variables in eq. 10 and 11 were kept constant during the 24-hours measurements. It also implicates that the two empirical correlations are very little sensitive to change of climate conditions of environment and are not suitable for analysis of tower performance in regards to daily and seasonal changes of ambient air. However, average values of Merkel number using both approaches do not differ significantly so all three equation are suitable for calculation of Merkel number for validation of results. It is important to notice that Merkel number according to eq. 9 takes into consideration both latent and sensible heat transfer via the difference of air enthalpy $i_{a,sat} - i_a$. It also reflects changes of ambient air and its curve follows the trends of thermal effectiveness and air wet bulb temperature shown in Fig. 5. This indicates that Merkel number could be valuable parameter to follow and possibly to try to keep within defined interval of values for ensuring optimal operating of cooling towers. However, it is important to note that Merkel's theory assumes same conditions of air at the inlet of tower fill as at the inlet of cooling tower (the ambient conditions) which can create non-negligible departure of results from real performance values. Some researches state that up to 10-20% of total heat exchange in cooling tower can happen inside of the rain zone (area under the packing in towers) [2]. This means that the parameters of air can significantly change during its flow through the rain zone before

entering the tower packing. Further investigation should take into consideration the heat transfer process in the rain zone and its effect on the Merkel's number. Moreover, the variations of air and mass flow rate would be of interest because these parameters are the ones to be used for controlling the process.

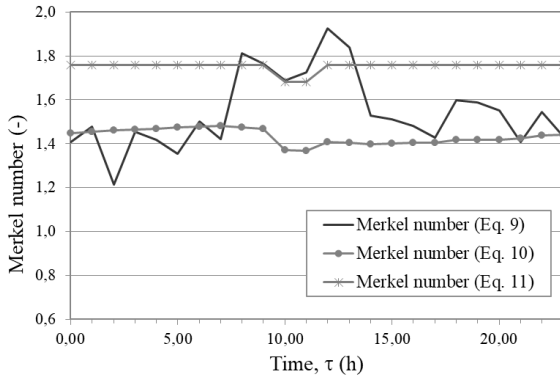


Figure 6. Merkel number

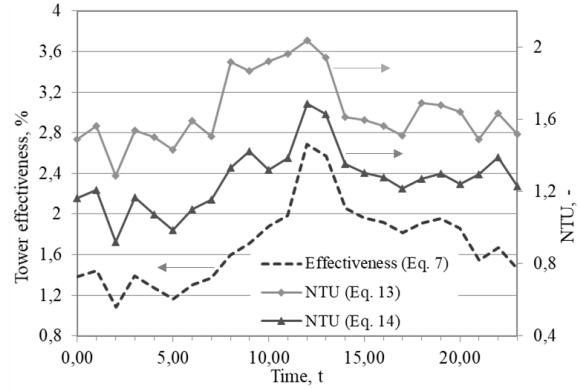


Fig 7. Tower effectiveness ε^* and NTU

4.3. Number of Transfer Units (NTU)

Value of Number of Transfer Units (NTU) is number of times that the average enthalpy potential ($i_{a,sat} - i_a$) goes into the temperature change of water (Δt_w) so it is a measure of the difficulty of the task [9]. According to ε -NTU approach [2], relation between NTU and Merkel number is given as:

$$NTU = \frac{di_a/dt_w}{c_{pw}} Me \quad \text{valid for conditions where } \dot{m}_a > \frac{\dot{m}_w \cdot c_{pw}}{di_a/dt_w} \quad (12)$$

Another formulation of NTU parameter is derived in [10] and it provides relation between tower effectiveness ε^* given by eq. (7) and NTU as:

$$NTU = \frac{\varepsilon^*}{Cro + 0.5 \cdot \varepsilon^* \cdot (Cro - \dot{m}_w/\dot{m}_a)} \quad (13)$$

where Cro is a function of interval of values for $t_{awb,in}$ and t_{win} . This approach as presented in [10] enables calculation of water outlet temperature once when NTU and \dot{m}_w/\dot{m}_a are known. Therefore, it is very convenient for optimisation of working mode of cooling towers.

The values of ε^* for selected time period of measurements show very good agreement with results of other authors. Therefore, value of ε^* is computed for 24h measurements period and it is used to calculate the values of NTU according to eq. 13. The value of Cro was chosen for the interval offered in [10], which was the closest to the measured values of temperature ranging from 16 °C to 36 °C, and it equals to 1.136. Values of calculated tower effectiveness ε^* and NTU for 24 hours measurements are given in Figure 7, together with NTU values calculated according to eq. (12). It is visible that they three have similar trends with maximum values which are reached at 12:00 h.

When compared to trends of climate parameters of air shown in Fig. 2, the relation between the NTU and wet bulb air temperature can be clearly noticed proving good sensitivity of this methods to the climate conditions of environment. Moreover, these methods also take into consideration the air and water mass flow rates which play important role in developing control methods. Therefore, the NTU

could be a good choice as a parameter to follow and try to keep in predefined interval by adjusting other parameters when possible. Which method should be used for NTU calculation will probably depend on the availability of measurement data in particular case but also, very importantly, on the fact which parameters of tower can be adjusted intentionally (e.g. air mass flow rate by changing the speed of fans).

4.4. Overall mass transfer coefficient

For known Merkel number, using eq. (8) it is possible to calculate mass transfer coefficient as:

$$h_d = Me \frac{\dot{G}_w}{a_{fi} \cdot L_{fi}} \quad (14)$$

Fill material installed in examined tower is PVC CHSB 21, with ratio $a_{fi} = A_p/V_c = 148 \text{ m}^2/\text{m}^3$ where A_p is the total area of the surface presented by the bed of packing and V_c is the column volume.

Empirical equation for overall heat and mass transfer coefficient, applicable for inlet water temperature ranging from 38-46 °C according to [8] is:

$$\beta_{xa} = A(w_a \cdot \rho_a)^m q^n \quad (15)$$

where β_{xa} is overall heat and mass transfer coefficient, ($\text{kgm}^{-3}\text{h}^{-1}$), w_a is air velocity calculated for the total section of the empty unit, (ms^{-1}), q is specific water volumetric flow rate, ($\text{m}^3\text{m}^{-2}\text{h}^{-1}$). Empirical coefficients are determined experimentally and have values of $A=635$, $m=0.53$ and $n=0.39$ [8].

Another empirical equation for counterflow cooling towers is presented in [4], for computing mass transfer coefficient per meter of fill height h_{dm} where values of all coefficients (a_d , b_{da} and b_{db}) are determined experimentally for different types of fill. When using values of coefficients for packing Brentwood Ind Accu-Pac CF 1900 [2] which is similar to packing used in the cooling towers in TPP Kakanj – Unit 7, the empirical equation is given as:

$$\frac{h_{dm} \cdot a_{fi}}{\dot{G}_w} = a_d \left(\frac{\dot{G}_w}{\dot{G}_a} \right)^{b_{da}} L_{fi}^{b_{db}} = 1.664 \left(\frac{\dot{G}_w}{\dot{G}_a} \right)^{-0.62} L_{fi}^{-0.27} \quad (16)$$

Measurements data are used to compute overall mass transfer coefficient by all three presented equations and the results for 24-hours period are given in Fig. 8. It is evident that all three equations resulted in relatively uniform values of overall mass transfer coefficient over the 24-hours period which indicates low sensitivity to variations of climate parameters of environment. Slightly more changes are provided by eq. 14 and it could be explained by the influence of Merkel number which is strongly dependent on climate conditions as shown before (eq. 9 and Fig. 6). The two empirical equations (eq. 15 and 16) are mostly determined by air and water mass flow rates so the only alteration in values happened around 10h when the water mass flow rate was slightly increased unexpectedly due to the current plant operation conditions. It is however curious that the results of eq. 15 differ significantly from other two sets of results and it could indicate that the correlation is not suitable for the examined towers or the measurement conditions. Further investigation should be performed for eq. 14 and 16 by testing other values of empirical coefficients and by introducing variations in air and/or mass flow rates.

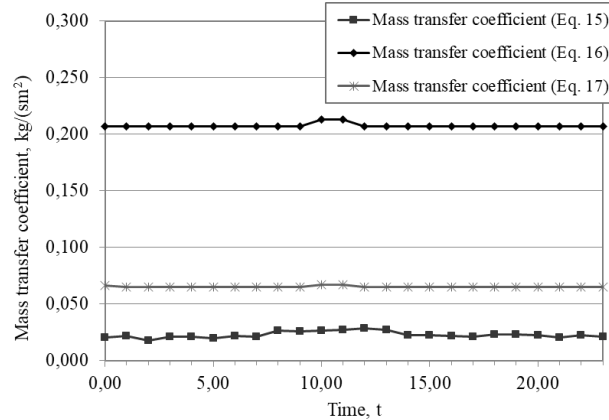


Fig 8. Mass transfer coefficient for 24-hours period of measurements

5. Conclusion

This paper presented values of different performance characteristics obtained by applying mathematical and empirical correlations on data from 24-hours measurement at operating cooling system of TPP Kakanj – Unit 7. Main focus of the paper was to analyse different parameters in regards to their sensitivity to climate parameters of environment which dictates condition for the performance of towers and of overall cooling system.

After performing necessary calculation and creating visual representation of results, it has been concluded that three parameters are sensitive to climate conditions of environment: thermal effectiveness, Merkel number (according to Merkel’s methods) and NTU. On the other hand, Merkel number and NTU could be easily linked to the air and water mass flow rates which are the controlled variables for cooling tower operation. Overall mass transfer coefficient by all three presented equations showed relatively low sensitivity to variations of climate parameters of environment. Further investigation with expanded measurements of varying air or mass flow rates could provide better insights in possibilities for improving tower operation control.

Limitations of this analysis are mainly related to the ones met during the measurements. The air and water mass flow rates were kept constant during the measurements which made it difficult to analyse the behaviour of some parameters. Further on, air mass flow rate for this research has been calculated based on the characteristics of fans which may not be as precise as needed. Also, water flow rate for one cooling tower is calculated by assuming even distribution of total water flow rate from condenser over the 10 operating cooling towers. Other limitations are related to model assumptions such as the one suggesting total saturations of air at tower outlet which can have great influence on fan speed control and its electricity consumption as well as on the drift water losses in tower.

Finally, expanded measurements in others seasons would provide complete picture of the tower behaviour. It would be important to learn about the performance of the towers during autumn regime when the relative air humidity can be high which decreases the evaporative heat rate in towers. Data about cooling system behaviour over the year would be of great value in designing detailed model sensitive to climate parameters of environment and providing good guidance on how to maintain optimal values of tower performance characteristics.

Nomenclature

a_{fi}	Transfer surface area per unit of volume (m^2m^{-3})
c_p	Specific heat at constant pressure ($Jkg^{-1}K^{-1}$)
\dot{G}	Mass velocity ($kgm^{-2}s^{-1}$)
h_d	Mass transfer coefficient ($kgm^{-2}s^{-1}$)
i	Enthalpy ($Jkg^{-1}K^{-1}$)
L_{fi}	Fill height (m)
\dot{m}	Mass flow rate ($kg s^{-1}$)
Me	Merkel number ($=h_d A/\dot{m}$) (-)
NTU	Number of Transfer Units (-)
p	Pressure (Pa or mbar)
t	Temperature ($^{\circ}C$)
Q	Heat rate (W)
x	Humidity ration ($kg_w kg_a^{-1}$)

Subscripts

a	Air (or dry bulb)
awb	Air wet bulb
$evap$	Evaporated
in	Inlet
lat	Latent
mp	Makeup water
out	Outlet
sat	Saturated
$sens$	Sensible
w	Water

Greek symbols

ε	Effectiveness
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