## NUMERICAL MODELLING OF LIQUID CO<sub>2</sub> PHASE TRANSITION BLASTING BASED ON SMOOTHED PARTICLE HYDRODYNAMICS ALGORITHM

#### by

## Zhanbiao YANG<sup>b,c</sup>, Yuejin ZHOU<sup>a\*</sup>, Xiaoding XU<sup>a\*</sup>, Wei YI<sup>a</sup>, Mingpeng LI<sup>a</sup>, and Xiaotong LI<sup>a</sup>

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 <sup>a</sup> State Key Laboratory for GeoMechanics and Deep Underground Engineering, China University of Mining and Technology, Xuzhou, Jiangsu, China
 <sup>b</sup> China Pingmei Shenma Group Institute of Energy and Chemical Industry, Pingdingshan, Henan, China
 <sup>c</sup> State Key Laboratory of Coking Coal Exploitation and Comprehensive Utilization, Henan, China
 <sup>d</sup> The Key Laboratory of Traffic and Transportation Security of Jiangsu Praince, Huaiyin Institute of Technology, Huaian, Jiangsu, China

> Liquid CO<sub>2</sub> phase transition blasting is a physical blasting method to enhance permeability through liquid  $CO_2$  phase transition expansion. To study the propagation criterion of fractures during blasting, the energy of phase transition blasting is evaluated through the thermodynamic equation by studying the action process of the liquid  $CO_2$  blasting, thus obtaining the scope of the smash zone and crack zone as well as the propagation criterion of fractures under the effect of high pressure gas. The gas blasting model for a coal body is established based on the SPH algorithm, thus obtaining the criteria for formation of the smash zone and for generatio and propagation of the crack zone. Moreover, the radius of phase transition blasting is surveyed onsite by the peephole method. It is shown that the explosive energy of the MZL-51/2000 phase transition blasting equipment with a release pressure of 270 MPa is 1510 kJ. The coal body is crushed by the high pressure  $CO_2$  percussive drilling, forming the smash zone. Meanwhile, fractures are generated around the smash zone. With the expansion and migratio of the gas, the fracture will further grow into a crack zone. The fracture inside the coal body goes through four states: rapid, slow, rapid, and then slow again. According to field surveys, the blasting radius of the *MZL-51/2000 equipment with loaded liquid of 1.8 kg is approximately 3 m.*

Key words: thermodynamics, phase transition blasting, gas blasting model propagation of fracture

#### Introduction

Rock blasting is a destructive process that features large-scale deformation and high strain rate under the effects of a dynamic load. Considering the complicated action process, numerical modelling is adopted by numerous scholars in rock blasting studies across the world. The finite element software program LS-DYNA was adopted by Wang [1] to simulate the tensile damage of underground explosions for brittle rocks and the wave propagation of jointed rocks during explosion was simulated [2]. A finite difference calculation program was developed [3] and used for calculations of the development and surface peeling-off of the fractures generated

<sup>\*</sup>Corresponding authors, e-mail: yuejinzh@163.com, ding\_xu@cumt.edu.cn

in rock blasting. These calculation results were compared with those obtained via LS-DYNA for analysis. The degree of damage of the rock mass exploited through blasting was researched by Pan et al. [4] through the continuous-discontinuous element method. The influence of different explosive payloads on the underground blasting effect was simulated and analyzed by Wei et al. [5] via the software program ANSYS-LSDYNA. Rock blasting was simulated by Ma et al. [6] through the Johnson-Holmquist model, and some suggestions were proposed for the engineering application of rock blasting. The generatio and propagation of fractures inside the rocks were simulated by Sivakumar et al. [7] via the finite element method. Some achievements have been made in numerical modelling of rock blasting, but most are based on rock damage due to stress waves, the expansion and migratio effect of high pressure gas is barely considered, so it is difficult to obtain the propagation criterion and distribution pattern of fractures. The smoothed particle hydrodynamics (SPH) algorithm, a mesh-free particle method, may overcome the deficiency of the finite element mesh method [8]. In this way, phenomena such as large-scale deformation, crushing and splashing of the materials during blasting and high-speed impact can be better simulated [9, 10]. In this paper, the blasting energy of phase transition blasting techniques is analyzed by means of the thermodynamic equation, and the propagation criterion of fractures during liquid CO<sub>2</sub> blasting is simulated and studied by using the SPH algorithm. Moreover, the radius of phase transition blasting is surveyed through onsite tests.

### Technical principle of liquid CO<sub>2</sub> phase transition blasting

## *Liquid* CO<sub>2</sub> *phase transition blasting equipment*

The liquid  $CO_2$  phase transition blasting equipment mainly includes a blasting tube, activating device, constant-pressure shear sheet, release tube, *etc.*, as shown in fig. 1.

The liquid  $CO_2$  is injected into the blasting tube through the filling system, and then the heating electrode is enabled by the initiation device. The chemicals inside the activating device are subject to rapid reaction after electrode heating, and then substantial heat is released, lead-



Figure 1. The main equipment of phase transition blasting

#### Energy analysis

Physical explosion is an extremely rapid energy release process, and the expansion of materials is converted into explosive energy by acting. The release form of energy includes the impact energy of high pressure gas, energy of debris and residual deformation energy of vessels. Because the blasting tube is made of high-strength steel, the deformation is subtle, and most energy is released in the form of the impact of high pressure gas.

In the case of phase transition blasting, the energy, *A*, of the entire system is evaluated by using the thermodynamic equation based on Helmholtz's free energy formula [8]:

$$A = u - Ts \tag{1}$$

ing to instantaneous gasification and expansion of the liquid  $CO_2$ . Once the pressure reaches the preset value, the constant-pressure shear sheet is fractured, and the gas erupts rapidly via the

gas vent of the release tube to realize the objec-

tive of blasting by acting on the coal body.

where T is temperature, s – the energy, and u – the internal energy.

The energy released from the explosion is expressed:

$$E = \int_{1}^{2} p \mathrm{d}V \cong -\Delta A \cong -\Delta u + T\Delta s \tag{2}$$

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Entropy will not be changed during the expansion of high pressure  $CO_2$ , so the energy released from the explosion is the decrement of internal energy. According to the gas state equation and law of thermodynamics, the internal energy, u, of unit mass of ideal gas is expressed:

$$u = \frac{1}{k-1} \mathbf{R}T \tag{3}$$

where k is the heat ratio heat capacity, k = cp/cv, cp – the isobaric heat capacity, cv – the isochoric heat capacity, and cp - cv = R.

Consequently, the energy released from an explosion can be expressed:

$$E = \int_{1}^{2} p \mathrm{d}V \cong -\Delta u \cong \frac{1}{k-1} \mathrm{R}T_{1} \left( 1 - \frac{T_{2}}{T_{1}} \right)$$
(4)

The change in entropy during gas expansion is expressed:

$$s_1 - s_2 = c_p \ln \frac{T_2}{T_1} - R \ln \frac{p_2}{p_1}$$
(5)

The change in isentropy is expressed:

$$\ln\frac{T_2}{T_1} = \frac{R}{c_p} \ln\frac{p_2}{p_1} \tag{6}$$

According to the definition of heat ratio heat capacity,  $R/c_p = (k-1)/k$  can be obtained:

$$\frac{T_2}{T_1} = \left(\frac{p_2}{p_1}\right)^{\frac{k-1}{k}} \tag{7}$$

Therefore, the explosive energy equation is:

$$E = \frac{1}{k-1} \mathbf{R} T_1 \left( 1 - \frac{T_2}{T_1} \right) = \frac{1}{k-1} p_1 V_1 \left[ 1 - \left( \frac{p_2}{p_1} \right)^{\frac{1}{k-1}} \right]$$
(8)

where E [kJ] is the explosion energy of gas,  $p_1$  [MPa] – the absolute pressure of gas inside the vessel,  $V_1$  [L] – the volume of the vessel, k – the specific heat ratio of gas,  $p_2$  – the absolute pressure of the external environment, taking the standard barometric pressure, and R – the gas constant.

The MZL-51/2000 fracturing tube is 2 m long, with an outer diameter of 51 mm and a volume of 2 L. The loaded liquid is approximately 1.8 kg. According to eq. (8), where the release pressure calculated is 270 MPa, the blasting energy is 1510 kJ.

## Analysis of fracture propagation mechanism

Analysis on fracture propagation under the effect of a stress wave

During propagation of the stress wave, the peak value of the wave is under constant attenuation, the rules of which can be expressed:

$$\sigma_{rd} = P\left(\frac{r_0}{r}\right)^{\omega} \tag{9}$$

where *P* is the initial incident pressure of the wave, *r* – the distance from some point of the rock to the center of boreholes,  $r_0$  – the radius of the borehole,  $\sigma_{rd}$  – the radial stress in some point of the rock, and  $\alpha$  – the attenuation coefficient of the stress wave,  $\alpha = 2 - \mu/(1 - \mu)$ .

At the boundary of the smash zone, the speed of the shock wave is attenuated into that of the stress wave, and the particle velocity ur is expressed:

$$u_r = \frac{c_p}{1+k} \tag{10}$$

where *k* is the isentropic coefficient.

According to the law of the conservation of momentum, the peak pressure,  $P_{\text{rmax}}$ , calculated at the boundary of the smash zone is expressed:

$$P_{r\,\max} = \rho c_p u_r \tag{11}$$

The calculated radius,  $R_0$ , of the smash zone of the coal body is expressed:

$$R_0 = r_0 \sqrt[\alpha]{\frac{P(1+k)}{\rho c_p^2}}$$
(12)

Under the effect of the shock wave, the coal body will be subject to damage to different extents. The attenuation coefficient,  $\alpha_D$ , of the stress wave considering the damage can be expressed:

$$\alpha_D = \frac{\alpha}{1 - D} \tag{13}$$

where D is the damage factor, and  $\alpha$  – the attenuation coefficient of the stress wave in the undamaged coal body.

The relationship between the dynamic radial stress  $\sigma rd$  and the dynamic circumferential stress,  $\sigma_{\theta d}$ , is expressed:

$$\sigma_{\theta d} = \frac{\mu}{1 - \mu} \sigma_{rd} \tag{14}$$

Considering the influence of damage on the strength of the coal body, the dynamic tensile strength of rocks can be expressed as  $\sigma_{td}(1-D)$ , so:

$$\sigma_{td}(1-D) = P(1-2b^2) \left(\frac{r_0}{r}\right)^{\alpha_D}$$
(15)

The calculated radius  $R_1$  of the crack zone is expressed:

$$R_{\rm l} = r_0 \, \frac{\alpha_0}{\sqrt{\sigma_{id} (1 - D)}} \tag{16}$$

### Analysis of the fracture propagation under the effect of high pressure gas

The acting duratio of high pressure gas on the coal body due to expansion inside the borehole is at least orders of magnitude over that of the stress wave. Because the pressure of high pressure gas is relatively stable, the action process can be deemed as a quasi-static process [11]. The stress intensity factor,  $K_I$ , of the macro fractures under the effect of high pressure gas is expressed:

$$K_{I} = 2\sqrt{\frac{a+r_{0}}{\pi}} \int_{0}^{a+r_{0}} \frac{P_{g}(x,t)}{\sqrt{(a+r_{0})^{2}-x^{2}}} dx$$
(17)

where  $P_g(x,t)$  is the pressure distribution of high pressure gas on the surface of macro fractures at time, *t*, and a is the length of macro fractures under the effect of ground stress, as shown in fig. 2.

The relationship between the pressure distribution of high pressure gas on the surface of macro fractures and the time variation is simplified:

$$P_g(x,t) = P(t)e^{-\alpha x}$$
(18)



Figure 2. The model of fracture propagation driven by high pressure gas

where P(t) is the pressure of high pressure gas inside the borehole [MPa], and  $\alpha$  – the attenuation coefficient of stress.

During liquid  $CO_2$  phase transition blasting, the length of fractures is far greater than the radius of the borehole, so the stress intensity factor,  $K_i$ , of the macro fractures under the effect of high pressure gas can be simplified as  $r_0 = 0$ :

$$K_{I} = 2\sqrt{\frac{a_{0}}{\pi}} \int_{0}^{a_{0}} \frac{P_{g}(x,t)}{\sqrt{a^{2} - x^{2}}} dx = \pi P(t)e^{-ab}\sqrt{\frac{a}{\pi}}$$
(19)

The development of the fracture tip is the consequence of constant accumulation of damage, so the effective stress intensity factor is defined to reflect the dynamic propagation process of fractures.

The effective stress intensity factor considering damage is expressed:

$$K_{I}^{*} = \frac{\pi P(t) e^{-ab} \sqrt{\frac{a}{\pi}}}{1 - D}$$
(20)

Assuming that the dynamic fracture toughness of the coal body is  $K_{DIC}$ , the stable propagation conditions of fractures can be expressed:

$$K_I^* \ge K_{DIC} \tag{21}$$

#### The SPH algorithm theory

The SPH algorithm is a Lagrange mesh-free algorithm proposed in the international community in recent years [12].

The equation of the SPH algorithm is generally carried out in two steps. The first step is the kernel approximation of the field function namely, approximating the field function via an integral representation:

$$f(x) \approx \int_{\Omega} f(x') W(x - x', h) dx'$$
(22)

where *h* is the smoothing length, determining the influence scope of W(x - x', h).

The second step is to separate the system into limited particles with independent mass and space, so the continuous integral representation of the SPH kernel approximation can be converted into a dispersed mode solving the sum of all particles in the domain.

$$f(x) = \int_{\Omega} f(x')W(x - x', h)dx' = \sum_{j=1}^{N} f(x_j)W(x - x_j, h)\frac{m_j}{\rho_j}$$
(23)

where N is the total number of particles in the area requiring solution,  $\rho_j$  – the density of particle *j*, and  $m_i$  – the mass of particle *j*.

#### **Constitutive Selection**

### The HJC constitutive model

The HJC model is composed of an equivalent strength model, state equation, and damage model [13]. The HJC equivalent strength model described by dimensionless equivalent stress can be expressed:

$$\sigma^* = \left\lceil A(1-D) + BP^{*N} \right\rceil (1 + C \ln \dot{\varepsilon}^*) \tag{24}$$

where  $\sigma^*$  is the dimensionless equivalent stress,  $P^*$  – the dimensionless pressure, P – the hydrostatic pressure,  $\dot{\varepsilon}^*$  – the dimensionless strain rate, D – the damage factor, and A, B, C, and N are material constants.



Figure 3. Changes in hydrostatic pressure with volumetric strain

The state equation is expressed in piecewise terms, indicating the changes in hydrostatic pressure with volumetric strain. The compression process is divided into three states: the elastic stress state, plastic state, and permanent densification state, as shown in fig. 3. The *P* is hydrostatic pressure,  $\mu$  – the volumetric strain of the rock,  $K_e$  – the bulk modulus of elasticity,  $\mu_{\text{crush}}$  – the elastic limit volumetric strain,  $P_{\text{crush}}$  – the hydrostatic pressure when the rock reaches its elastic limit,  $K_{\text{crush}} = (P_{\text{lock}} - P_{\text{crush}})//(\mu_{\text{lock}} - \mu_{\text{crush}})$ ,  $\bar{\mu}$  – the corrected volumetric strain,  $\mu_{\text{lock}}$  – the corresponding volumetric strain of the permanent densification limit, and  $K_1, K_2$ , and  $K_3$  are pressure constants.

Damage variable, *D*, is obtained through the accumulation of equivalent plastic strain and plastic volumetric strain, whose damage evolution equation is as:

$$D = \sum \frac{\Delta \varepsilon_p + \Delta \mu_p}{\varepsilon_p^f + \mu_p^f}$$
(25)

By leveraging the tests of uniaxial compression, tensile splitting strength, and other tests for coal, the physical and mechanical parameters of coal are obtained as: elastic modulus E = 2.47 GPa, poisson's ratio  $\mu = 0.3$ , compressive strength  $f_c = 16.32$  MPa, tensile strength T = 1.34 MPa, and density  $\rho_0$  is 1400 kg/m<sup>3</sup>. In addition, shear modulus G and bulk modulus  $K_e$  of coal can be obtained:

$$G = \frac{E}{2(1+\mu)} = 0.95 \text{ GPa}$$
 and  $K_e = \frac{E}{3(1-2\mu)} = 2.06 \text{ GPa}$ 

The corresponding volumetric strain and hydrostatic pressure when the material reaches its elastic limit can be obtained according to the following equations:

$$P_{\text{crush}} = \frac{f_c}{3} = 3.44 \text{ MPa}, \quad \mu_{\text{crush}} = \frac{P_{\text{crush}}}{K_e} = 0.0017$$

At dimensionless tension  $T^* = T/f_c = 0.11$ , damage factor  $D_I = 0.01/(1/6 + T^*) = 0.036$ . Damage factor,  $D_2$ , has little influence on the model results [14]. Therefore,  $D_2 = 1$  according to the literature [14].

Xie [15] indicated that the densification density of the coal rock test  $\rho_{\text{grain}} = 1631 \text{ kg/m}^3$ , and the volumetric strain of the densification limit  $\mu_{\text{lock}} = \rho_{\text{grain}}/\rho_0 - 1 = 0.14$ . The  $K_1, K_2$ , and  $K_3$  can be determined according to the Hugoniot shock test or taken from the literature [16] in the absence of test data:  $K_1 = 85$  GPa,  $K_2 = -171$  GPa, and  $K_3 = 208$  GPa. According to Xie [15], take  $P_{\text{lock}} = 1$  GPa, A = 0.4, B = 0.7, C = 0.005, and N = 0.5.

#### State equation of high pressure gas

The JWL state equation may describe an explosion without chemical reaction and accurately reflect the expansive driving process of blasting products [17]. Therefore, the following JWL state equation can be used as the  $CO_2$  state equation. The JWL state equation is:

$$P = A \left( 1 - \frac{\omega}{R_{\rm I}V} \right) {\rm e}^{-R_{\rm I}V} + B \left( 1 - \frac{\omega}{R_{\rm 2}V} \right) {\rm e}^{-R_{\rm 2}V} + \frac{\omega E}{V}$$
(26)

where P is the pressure of blasting products, V – the relative specific volume, E – the internal energy of blasting products per unit volume, and A, B,  $R_1$ ,  $R_2$ , and  $\omega$  are parameters to be determined.

When the release pressure of the constant-pressure shear sheet is 270 MPa, the energy released from the explosion of liquid CO<sub>2</sub> fracturing equipment is approximately 1510 kJ. With reference to the state equation of blasting products generated by TNT, taking  $A = 3.73 \times 1011$ ,  $B = 3.75 \times 109$ ,  $R_1 = 4.15$ ,  $R_2 = 0.9$ ,  $\omega = 0.35$ , and  $E = 6 \times 109$ , the high pressure radius gas is 6 mm.

# Numerical modelling of phase transition blasting

Liquid CO<sub>2</sub> blasting of a coal body is a highly non-linear dynamic process at a high strain rate. It is easy to generate mesh distortion and terminate the calculation using a conventional Lagrange algorithm. Meanwhile, considering the expansion and migratio of high pressure gas, the SPH algorithm is adopted to model the liquid CO<sub>2</sub> blasting process of a coal body.

In the numerical modelling, the geometric size of the coal body is  $10 \text{ m} \times 10 \text{ m}$ , and there is a round borehole with a diameter of 75 mm in the center, as shown in fig. 4. The constitutive model is the HJC model and is added to the maximal tension stress failure criterion. Both the coal body and high pressure gas are modeled using the SPH algorithm, and their numbers of particles are 110764 and 592, respectively. The monitoring points are set at 0.3 m, 0.5 m, 1 m, 1.5 m, 2 m, and 2.5 m from the borehole on the right.



Figure 4. Numerical model of liquid CO<sub>2</sub> blasting



Figure 5. Final distribution pattern of blasting fractures; (a) numerical modelling of fracture distribution, (b) test of fracture distribution

The modelling results of fracture distribution of the coal body after liquid  $CO_2$  blasting are shown in fig. 5.



Figure 6. Complete evolution process of blasting fractures; (a) t = 0.2 ms, (b) t = 0.72 ms, (c) t = 1.82 ms, (d) t = 2.87 ms (e) t = 3.3 ms, and (f) t = 3.49 ms



Figure 7. Relationship between fracture length and time

The complete fracture evolution process in the phase transition blasting process is shown in fig. 6.

The reflected stress wave generates a tension effect on the fractures, and the fracturepropagation speed changes dramatically, as shown in fig. 7.

Figure 8 shows that the speed of the particles near the borehole increases rapidly at the early stage of blasting. Figure 9 indicates the relationship between the monitoring point position and the peak speeds at monitoring points and their corresponding time points.

# Survey and test of blasting radius

A radius survey and test were carried out in the air return channel of the working surface. Boreholes with a diameter of 75 mm and depth of 60 m were arranged at either side of the undrained mining area. Moreover, three holes were drilled at the left and right sides of the blasting hole as peepholes. The distances from the peepholes to the blasting hole were set to 1.5 m, 2 m, 3 m, 3.5 m, 4 m, and 5 m in sequence. The lay-out of boreholes is shown in fig. 10. The loaded liquid of the MZL-51/2000 fracturing equipment was 1.8 kg, and the release pressure of the constant-pressure shear sheet was 270 MPa. Linkages within the blast-

ing hole and the blasting equipment were uniformly arranged at a ratio of 1:1, with a hole sealing length of 15 m.



Figure 8. Relationship between speed at monitoring point and time



Figure 9. Relationship between the monitoring point position and the peak speeds at monitoring points and their corresponding time points

The peeping instrument was used to observe the crushing of the coal bed inside the boreholes. The observation results of boreholes  $G_3$  and  $G_4$  are shown in fig. 11.

It can be seen in fig. 11 that borehole  $G_3$  has a smooth wall before phase transition blasting, and there are only a few small cracks in the coal body.

#### Conclusions

Through studying the action process of liquid  $CO_2$  blasting, the energy of phase transition blasting is evaluated using a thermodynamic equation, and an explosion energy equation is established. The explosion energy of MZL-51/2000 liquid  $CO_2$  phase transition blasting equipment at 270 MPa is calculated to be 1510 kJ.



Figure 10. Schematic diagram for lay-out of boreholes



Figure 11. Borehole view; (a) before blasting of  $G_3$ , (b) after blasting of  $G_3$ , (c) before blasting of  $G_4$ , and (d) after blasting of  $G_4$ 

According to the form of the damage, the smash zone, crack zone, and tension crack zone are roughly formed after coal body blasting. Liquid  $CO_2$  leads to the formation of a limited smash zone on the inner wall of the borehole under the action of instant thermal expansion. Subsequently, under the joint action of the stress wave and high pressure gas, the crack zone connected with the smash zone is formed. The stress wave reflected from the boundary is converted into a tensile wave, which continues to generate tension cracks at the boundary of the coal body.

The phase transition blasting of the coal body is modeled based on the SPH algorithm to simulate the liquid  $CO_2$  phase transition blasting, analyze the formation Mechanism of cracks in the blasting process, and obtain the laws for formation of the smash zone around the borehole as well as generatio and expansion of the crack zone.

The radius of phase transition blasting is surveyed by using the peephole method. The blasting radius of the MZL-51/2000 phase transition blasting equipment with 1.8 kg of loaded liquid is approximately 3 m.

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#### Nomenclature

- E explosion energy of gas, [kJ]
- K specific heat ratio of gas, [-]
- P initial incident pressure of the
- wave, [MPa] P(t) – pressure of HP gas inside the
- borehole, [MPa]  $p_1$  – absolute pressure of gas inside
- the vessel, [MPa]
- *p*<sub>2</sub> absolute pressure of the external environment, [MPa]

- R gas constant, [-]
- *r* distance from some point of the rock to the center of boreholes, [m]
- $r_0$  radius of the borehole, [m]
- $V_1$  volume of the vessel, [L]

#### Greek symbols

- $\alpha$  attenuation coefficient of stress, [MPa]
- $\sigma_{rd}$  radial stress in some point of the rock, [-]

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