

## A NOVEL SOLUBILITY MODEL IN A SUPERCRITICAL CO<sub>2</sub>

by

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*This paper gives a semi-empirical formula for calculation of solubility of dyestuff in a supercritical CO<sub>2</sub> by dimensionless analysis, the obtained scaling law reveals that the solubility depends mainly on pressure and density of the supercritical CO<sub>2</sub>.*

Key words: *solubility, dyestuff, supercritical CO<sub>2</sub>, scaling law, Bernoulli equation*

### Introduction

Supercritical CO<sub>2</sub> is a green solvent, and it is widely used in supercritical fiber dyeing process [1-4]. Senyay-Oncel and Yesil-Celiktas [5] studied activity enhancement of cellulose treated with supercritical CO<sub>2</sub>, and found that enzymes as catalysts in biochemical applications can be greatly improved by using supercritical fluids as potential media. Russler *et al.* [6] studied different approaches towards hydrophobic modification of bacterial cellulose aerogels with the alkyl ketene dimer (AKD) reagent, and found that if AKD modification was performed in supercritical CO<sub>2</sub>, an unexpectedly high degree of loading was observed. However, the dye solubility in the supercritical CO<sub>2</sub> keeps still an open problem, though there are many semi-empirical formulae for this purpose [7-11]. For example:

$$T \ln(y_2 p) = a_1 + a_2 \rho + a_3 T \quad (1)$$

$$\ln(y_2) = A + \frac{B}{T} + C \rho \quad (2)$$

$$\ln(y_2) = A' + \frac{B'}{T} + \left( C' + \frac{D'}{T} \right) \ln \rho \quad (3)$$

where  $y_2$  is the solubility of dyestuff in mole fraction,  $T$  – the temperature,  $p$  – the pressure,  $\rho$  – the density of supercritical CO<sub>2</sub> [12], and the parameters in previous equations are constants, which can be determined experimentally. Equation (1) is the Mendez-Santiago-Teja

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formula [7], eq. (2) is the Kumar-Johnston formula [8], and eq. (3) is the Sung-Shim formula [9]. Though semi-empirical ones were widely used in supercritical fiber dyeing process, but all parameters in previous formulae are not dimensionless ones. Dimensionless analysis [13-15] should be adopted in the derivation of the semi-empirical formulae.

### Dimensionless analysis

Dimensionless analysis has been widely applied in engineering to derive an empirical formula [13]. The solubility of dyes in supercritical CO<sub>2</sub> is a function of pressure, density and velocity of the supercritical CO<sub>2</sub>:

$$y_2 = y_2(p, \rho, u) \quad (4)$$

Temperature is also a main factor affecting the solubility indirectly, it affects the density directly, so temperature is not involved in eq. (4).

By dimensionless analysis method, we write:

$$y_2 \propto p^a \rho^b u^c \quad (5)$$

where  $a$ ,  $b$ , and  $c$  are constants. Balancing the dimensions of previous equation, we have:

$$[ML^{-3}] = [ML^{-1}T^{-2}]^a [ML^{-3}]^b [LT^{-1}]^c \quad (6)$$

or

$$\begin{cases} 1 = a + b \\ -3 = -a - 3b + c \\ 0 = -2a - c \end{cases} \quad (7)$$

Solving eq. (7), we have  $a = n$ ,  $b = 1 - n$ ,  $c = -2n$ , where  $n$  is a free parameter. So the solubility scales as:

$$y_2 \propto p^n \rho^{1-n} u^{-2n} \quad (8)$$

Therefore, we obtain a scaling law for solubility of dyestuff in a supercritical CO<sub>2</sub>, which is:

$$y_2 \propto \left(\frac{\Pi}{E}\right)^n \rho \quad (9)$$

where  $\Pi = p/\rho$  and  $E = 1/2u^2$ . According to Bernoulli equation, we have:

$$\Pi + E = B \quad (10)$$

where  $B$  is a Bernoulli constant. Equation (9) becomes:

$$y_2 \propto \left(\frac{\Pi}{B - \Pi}\right)^n \rho \quad (11)$$

or

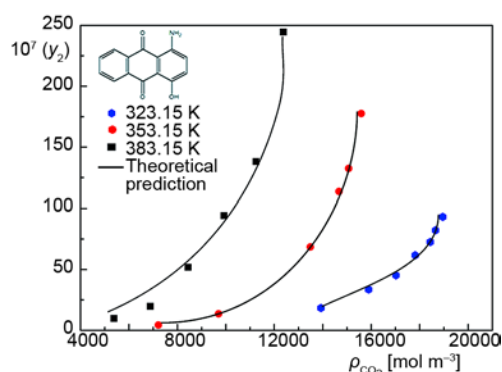
$$y_2 = \alpha + \beta \left( \frac{\Pi}{B - \Pi} \right)^n, \quad \rho = \alpha + \beta \left( \frac{P}{B\rho - P} \right)^n, \quad \rho = \alpha + \beta \left( \frac{P}{\frac{P_0\rho}{\rho_0} - P} \right)^n \quad (12)$$

where  $\alpha$  and  $\beta$  are constants,  $P_0$  and  $\rho_0$  – the pressure and density, respectively, when the velocity is zero.

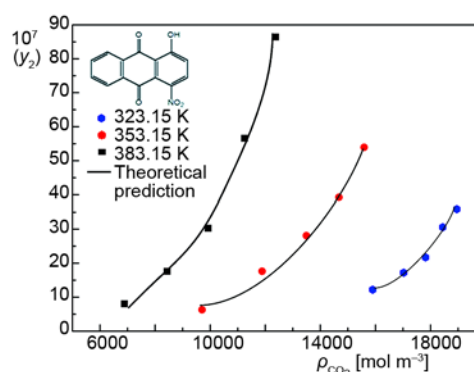
Table 1 shows the parameters and the average absolute relative deviation (AARD) between the measured and predicted results. Figures 1 and 2 compare our theoretical prediction with experimental data from [10].

**Table 1. Parameters of eq. (12) and AARD between the experimental and predicted results**

System	Parameters				AARD/%
	$\alpha \cdot 10^4$	$\beta \cdot 10^5$	$n \cdot 10^3$	$P_0/10^7$ [MPa]	
1-amino-4-hydroxyanthraquinone	-0.10236	1.1545	-1.9769	0.6793	7.36
1-hydroxy-4-nitroanthraquinone	-7.052	0.6236	-423	0.9217	5.6



**Figure 1. Comparison of solubilities of 1-amino-4-hydroxyanthraquinone in supercritical CO<sub>2</sub> with experimental data [10]**



**Figure 2. Comparison of solubilities of 1-hydroxy-4-nitroanthraquinone in supercritical CO<sub>2</sub> with experimental data [10]**

## Conclusion

We obtain a semi-empirical formula, eq. (12), for calculation of solubility of dye-stuff in a supercritical CO<sub>2</sub> by dimensionless analysis. Using the state equation for supercritical CO<sub>2</sub> [10], temperature can be involved in eq. (12). Though the dimensionless analysis has been practiced many times in various fields, theoretical or experimental verification of eq. (12) is still much needed.

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