

CONDENSATE RETENTION AS A FUNCTION OF CONDENSATE FLOW RATE ON HORIZONTAL ENHANCED PIN-FIN TUBES

Hafiz Muhammad ALI^{1,*}, Hassan ALI², Muhammad ABUBAKER³, Ahmed SAIIEED⁴, William PAO⁴, Majid AHMADLOUYDARAB⁵, Hasan KOTEN⁶, Muhammad ABID³

¹ Mechanical Engineering Department, University of Engineering and Technology, Taxila, 47050, Pakistan

² Faculty of Mechanical Engineering, University of Engineering and Technology, Lahore, Pakistan

³ Department of Mechanical Engineering, COMSATS Institute of Information and Technology, Sahiwal, Pakistan

⁴ Mechanical Engineering Department, Universiti Teknologi PETRONAS, 32610 Seri Iskandar, Perak Darul Ridzuan, Malaysia

⁵ Faculty of Chemical & Petroleum Engineering, University of Tabriz, 51666-16471, Iran

⁶ Mechanical Engineering Department, Istanbul Medeniyet University, Istanbul, 34700, Turkey

*h.m.ali@uettaxila.edu.pk

The extent of condensate flooding as a function of condensate flow rate is measured on six horizontal pin-fin tubes (varying in circumferential pin-spacing) via simulated experimentation. Surface tension to density ratio is tested using three fluids namely water, ethylene glycol and R-141b. Results show that flooding was strongly effected by changing the condensate flow rate. An increase in flow rate caused a marginal decrease in flooding angle (an angle extracted from top of the test tube to the fully flooded flank). Similarly, circumferential pin-spacing also effected the retention angle and the effect goes on increasing by decreasing the surface tension to density ratio.

Keywords: *Condensate; Retention; Pin-Fin tube; Flow rate, Heat transfer*

1. Introduction

The phenomenon of condensation has vital role in many engineering applications. Soon after the realization of heat transfer enhancement based on available surface area, simple plain condensing tubes were replaced by two-dimensional integral-fin tubes. However, due to surface tension effects, an adequate amount of condensate was observe to retain in between the fins, a phenomenon first observed by Katz et. al., [1]. The extent of this flooding is measured by retention angle which is measured from top of the tube to the full flooded flank between the inter-fin spacing.

A comprehensive experimental data on heat transfer is available on integral-fin tubes [2-8]. Researchers also compared the measured retention angle in actual condensation with static condensation and no appreciable change was noted. Reasonable heat transfer models have also been reported [9-11] in which retention angle was found main parameter in the measurement of heat transfer.

Retention angle measurement based on vapour velocity has also been reported on integral-fin tubes [4, 12] and a semi-empirical model was reported by Ali and Amanat [12] which agree to data for water, ethylene glycol and R-141b to within ± 20 %.

42 After the advancement in tube geometry, trend shifted to more sophisticated three-dimensional
43 tubes also known as pin-fin tubes. A reasonable heat transfer data is now available which shows the
44 superior performance of these tubes over integral-fin tubes [13-21] and reports the effect of pin
45 geometry over a range of fluids successfully. Recently Ali and Briggs [20] published an analytical
46 model which predict most of the experimental data on pin-fin tubes to within $\pm 15\%$. Ali also
47 summarized the previous work on enhanced tubes successfully [22].

48 Effect of vapour velocity on condensate retention was studied systematically by Ali and
49 Abubaker [23, 24]. Geometric parameters varied were circumferential pin spacing and circumferential
50 tooth thickness. In all cases, pin-fin tubes were found less flooded when compared with equivalent
51 integral-fin tube.

52 Eight horizontal tubes varying in fin spacing were tested under static condensation [25]. Three
53 fluids namely water, ethylene glycol and R-141b were tested. Data showed the independence of the
54 effect of mass flow rate on the retention angle.

55 Based on the literature review available, only one study of Ali et. al., [25] is available which
56 reports the effect of condensate flow rate on integral-fin tubes. In this paper pin-fin tubes are tested
57 under static condensation and the effect of mass flow rate on these tubes is presented.

58 2. Methodology

59 Simulated experimentation was accomplished with small holes (about 0.4 mm in diameter) in
60 between the rectangular fins in longitudinal direction. One end of the tube was connected to a fluid
61 reservoir via a flexible tube and a needle valve to control the flow rate. The tube under test was located
62 horizontally such that the small holes were kept right at the top. The schematic of experimental set-up
63 and test tubes can be seen in Fig. 1 and 2 respectively.

64 Three fluids namely water, ethylene glycol and R-141b were tested. Colored dye was also
65 mixed with first two fluids in order for quick recognition of the flooding point. The fact that
66 measurements with almost zero condensate flow rate agreed closely with Eq. of Honda et al. [2],

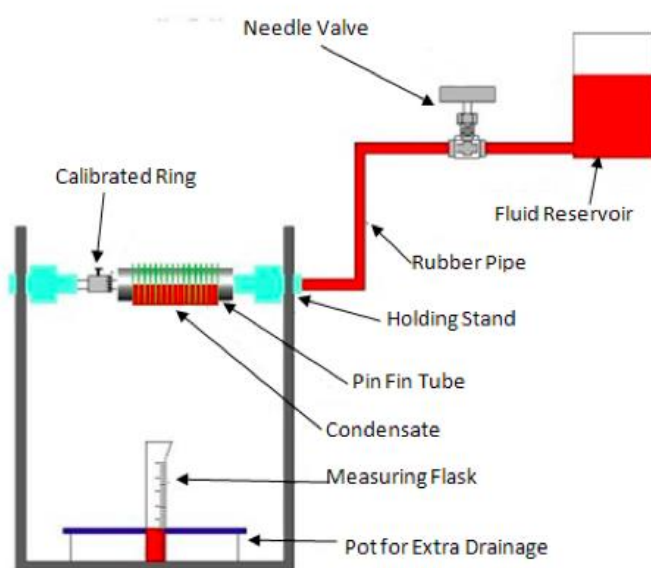


Figure 1. Schematic of Apparatus

shows that adding small amounts of food coloring did not affect the surface tension significantly. As R-141b doesn't dissolve the dye, careful observation was made while locating the point to which fins were flooded.

Retention angle was measured using calibrated ring method. Pin fin tubes were mounted horizontally with a calibrated ring having angles from zero to 360 degree marked on it (see Fig. 3). This ring made up of aluminum was mounted on

84 the finless portion of the tube. Ring had the inner diameter a 12.7 mm same as the fin root

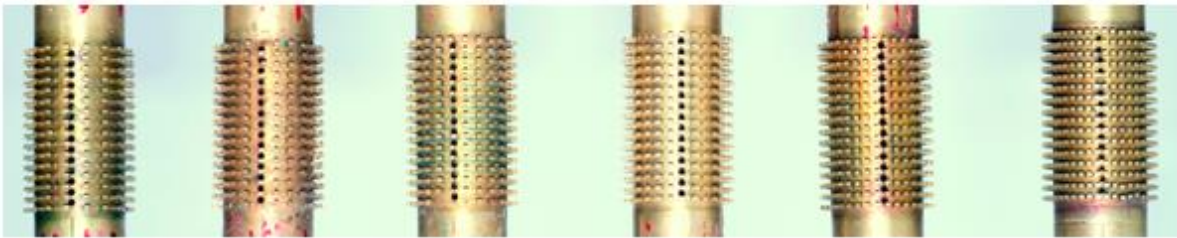


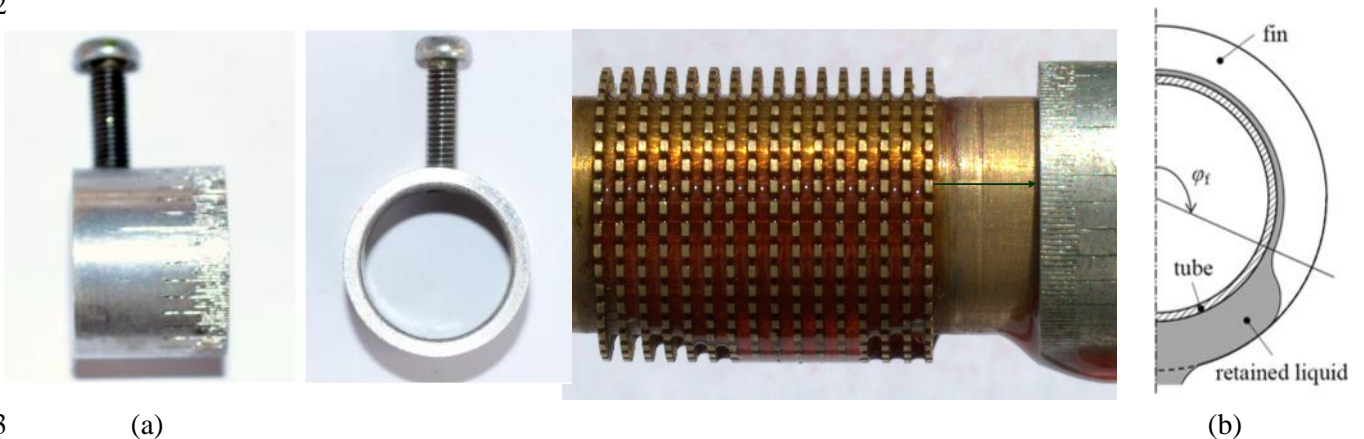
Figure 2. Pin-Fin tubes used in the present experiment

85 diameter with a small tolerance so that it may slide over the tube. Zero error was done by
86 adjusting the small holes aligned with the zero degree of calibrated ring.

87

88 Once the error is removed the screw at the top of calibrated ring was tightened. The retention
89 angle was then measured with the help of that ring as shown in Fig 3. The results were also compared
90 with photographic method and good agreement was found (see sample of photographs in Fig. 4 and 5).
91 The accuracy of calibrated ring method was around ± 6 degrees.

92



93

(a)

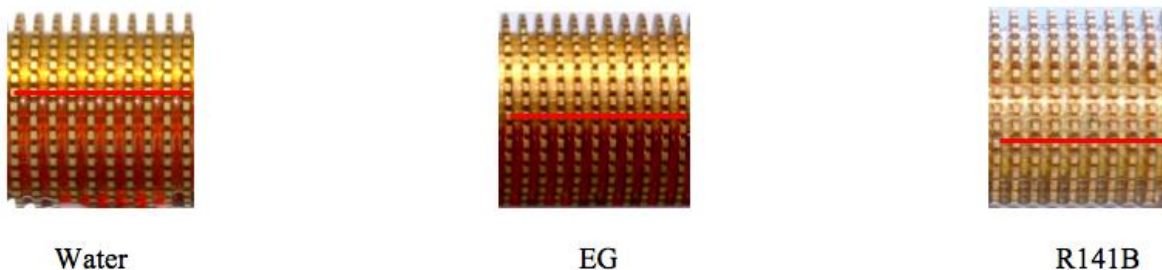
(b)

Figure 3 (a). Calibrated ring for the measurement of condensate retention angle.

(b). Condensate retention angle.

94 The flow rate was adjusted so that the fluid spilled steadily and uniformly over the tube surface.
95 Photographs were taken for each tube at the flow rate starting from nearly zero flow rate which was
96 attained by spraying the condensate over the tube and measuring the retention angle, and ending at the
97 flow rate at which the tube gets fully flooded. Measuring flask and stop watch were used to measure
98 flow rate.

99



100

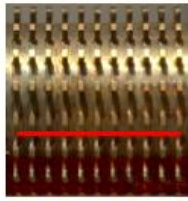
Water

EG

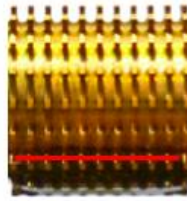
R141B

Figure 4. Photographs of test tube T0 with minimum flow rate (Lines show the retention angles)

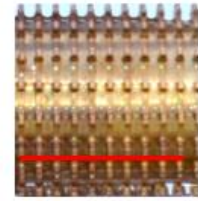
101



Water



EG



R141B

102

Figure 5. Photographs of test tube T5 with minimum flow rate (Lines show the retention angles)

103

Table 1. Dimension of test tubes used in the present investigation in mm

| Tubes | $t_c(\text{root})$ | $t_c(\text{tip})$ | s_c | t | s | h | d_r | d_o |
|-------|--------------------|-------------------|-------|-----|-----|-----|-------|-------|
| T0 | 0.4 | 0.62 | 0.5 | 0.5 | 1 | 1.6 | 12.7 | 15.9 |
| T1 | 0.36 | 0.62 | 0.75 | 0.5 | 1 | 1.6 | 12.7 | 15.9 |
| T2 | 0.33 | 0.64 | 1.0 | 0.5 | 1 | 1.6 | 12.7 | 15.9 |
| T3 | 0.28 | 0.65 | 1.25 | 0.5 | 1 | 1.6 | 12.7 | 15.9 |
| T4 | 0.23 | 0.64 | 1.5 | 0.5 | 1 | 1.6 | 12.7 | 15.9 |
| T5 | 0.22 | 0.74 | 2 | 0.5 | 1 | 1.6 | 12.7 | 15.9 |

104

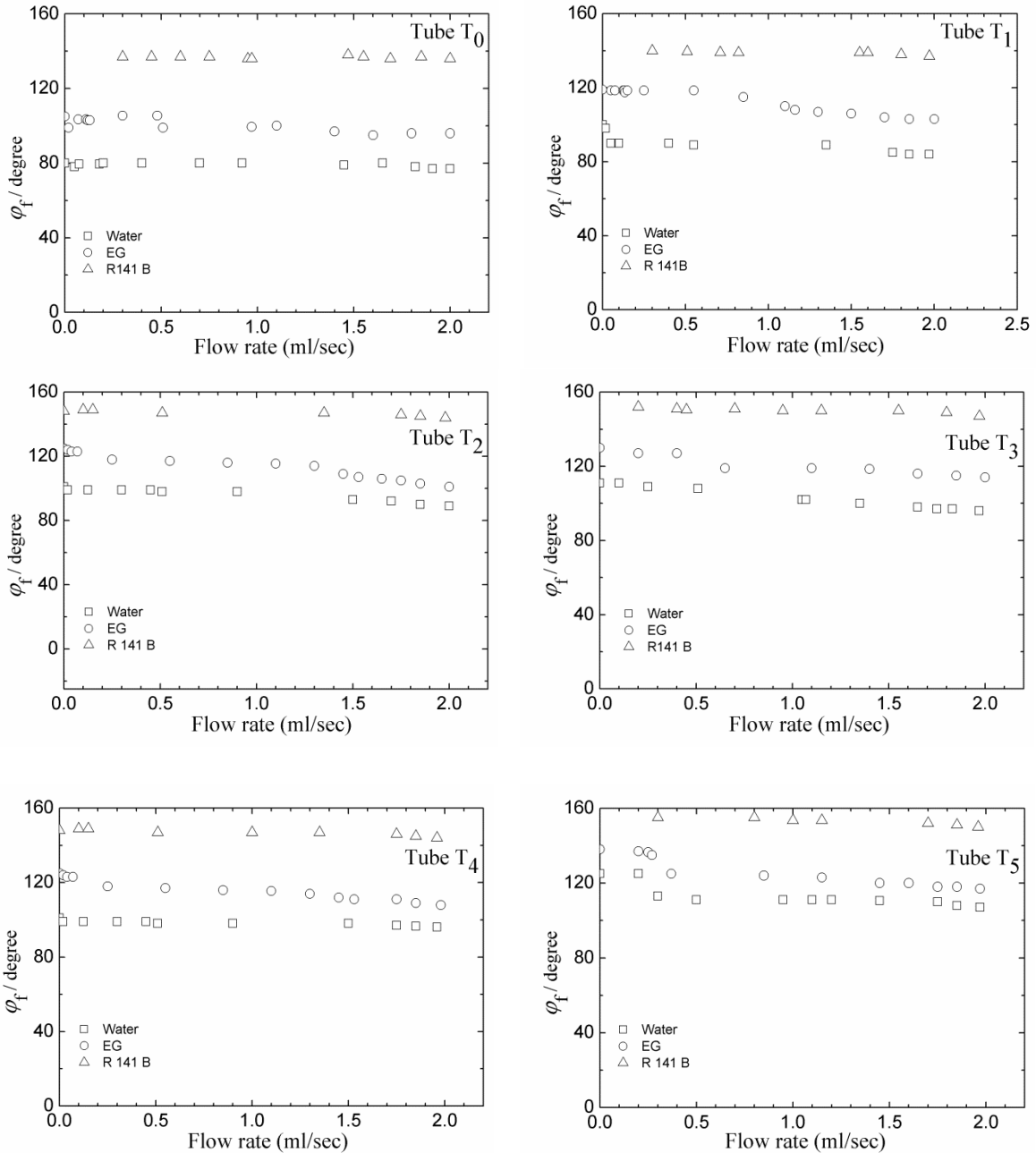
105 3. Results and Discussion

106 Graphs for condensate retention angle versus condensate flow rate are shown in Figure 6. The
 107 difference in condensate retention angle between water and R141B at zero condensate flow rate is
 108 around 60 for circumferential pin spacing of 0.5 mm (T0). However, this value reduces to around 40
 109 for for circumferential pin spacing of 2 mm (T5). It is interesting to note that variation in retention
 110 angle with changing circumferential pin spacing is more significant for liquids with higher surface
 111 tension to density ratio such as water. The results could also be used to estimate the condensate
 112 retention angles for liquids with different surface tension to density ratios at different condensate flow
 113 rates.

114 For all tubes tested the condensate retention angle has remained constant for a range of
 115 condensate flow rate (0 – 2 ml/sec). This highlights the importance and usefulness of pin fin tubes in
 116 industrial condensers, where tube banks are used. For the case of smooth and finned tubes, significant
 117 degradation in heat transfer is obtained on the lower tubes in the bank. Firstly, higher condensate
 118 retention angles are obtained as lower tubes get thoroughly inundated with the condensate falling from
 119 the higher tubes. Secondly, condensate retention angles increase as vapour velocity is decreased,
 120 consequently shearing effect of vapour velocity is reduced.

121 Figure 7 shows the variation of retention angle with surface tension to density ratio. At a
 122 particular value of surface tension to density, variation in condensate retention angle is due to variation
 123 in circumferential pin spacing. Higher condensate retention angles correspond to higher
 124 circumferential fin spacing.

125 This data could be used to determine the retention angle on pin-fin tubes for different liquids
 126 with a range of surface tension to density ratios.



127

Figure 6. Effect of condensate flow rate on test tubes using water, ethylene glycol and R-141b as test fluids

128
129
130
131
132
133

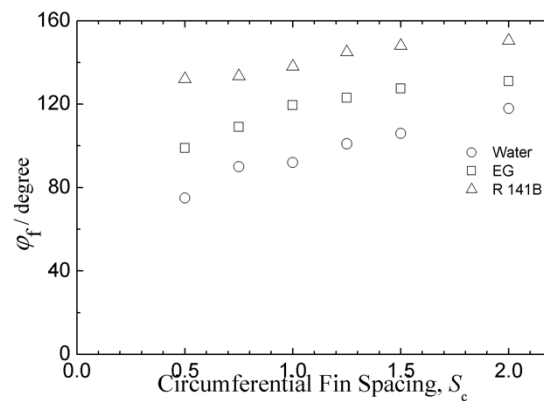


Figure 7. Effect of surface tension to density ratio on retention angle with minimum flow rate

134 4. Conclusions

135 New experimental data has been reported to determine the retention angle characteristics for
136 simulated condensation of water, ethylene glycol and R141B as a function of condensate flow rate.
137 Based on the findings it is recommended that the pin-fin tubes could be used in the bank of tubes that
138 get thoroughly inundated. Since, no drainage mechanism is present for the case of smooth tubes,
139 significant reduction in heat transfer is observed. Results for a range of condensate flow rates have
140 been supportive of the fact that pin fin tubes could be used in the bank of tubes in general and lower
141 the bank in particular.

142 Moreover, for optimised geometries, further investigation is needed to determine the retention
143 angle and heat transfer characteristics for a range of condensate flow rates and geometries.

144

145 Acknowledgments

146 The corresponding author wishes to acknowledge the financial support provided by the
147 University of Engineering and Technology, Taxila, Pakistan under the faculty research project
148 through approval letter No. UET/ASR&TD/RG-1001.

149

150 References

151

- 152 [1] D. Katz, R. Hope, and S. Datsko, "Liquid retention on finned tubes," *Dept. of Eng. Research,*
153 *Univ. of Michigan, Ann Arbor, MI, Project M*, vol. 592, p. 1946, 1946.
- 154 [2] H. Honda, S. Nozu, and K. Mitsumori, "Augmentation of condensation on horizontal finned
155 tubes by attaching a porous drainage plate," in *Proc. ASME-JSME Thermal Engineering Joint*
156 *Conference*, 1983, pp. 289-296.
- 157 [3] T. Rudy and R. Webb, "An analytical model to predict condensate retention on horizontal
158 integral-fin tubes," *Journal of heat transfer*, vol. 107, pp. 361-368, 1985.
- 159 [4] C. L. Fitzgerald, A. Briggs, J. W. Rose, and H. S. Wang, "Effect of vapour velocity on
160 condensate retention between fins during condensation on low-finned tubes," *International*
161 *Journal of Heat and Mass Transfer*, vol. 55, pp. 1412-1418, 2012.
- 162 [5] K. Yau, J. Cooper, and J. Rose, "Horizontal plain and low-finned condenser tubes—effect of
163 fin spacing and drainage strips on heat transfer and condensate retention," *Journal of heat*
164 *transfer*, vol. 108, pp. 946-950, 1986.
- 165 [6] A. Wanniarachchi, P. Marto, and J. Rose, "Film condensation of steam on horizontal finned
166 tubes: effect of fin spacing," *ASME Journal of Heat Transfer*, vol. 108, pp. 960-965, 1986.
- 167 [7] A. Briggs, X.-L. Wen, and J. Rose, "Accurate heat transfer measurements for condensation on
168 horizontal, integral-fin tubes," *Journal of heat transfer*, vol. 114, pp. 719-726, 1992.

- 169 [8] K.-J. Park and D. Jung, "Optimum fin density of low fin tubes for the condensers of building
170 chillers with HCFC123," *Energy Conversion and Management*, vol. 49, pp. 2090-2094, 2008.
- 171 [9] H. Honda and S. Nozu, "A prediction method for heat transfer during film condensation on
172 horizontal low integral-fin tubes," *Journal of heat transfer*, vol. 109, pp. 218-225, 1987.
- 173 [10] J. Rose, "An approximate equation for the vapour-side heat-transfer coefficient for
174 condensation on low-finned tubes," *International journal of heat and mass transfer*, vol. 37,
175 pp. 865-875, 1994.
- 176 [11] A. Briggs and J. Rose, "Effect of fin efficiency on a model for condensation heat transfer on a
177 horizontal, integral-fin tube," *International journal of heat and mass transfer*, vol. 37, pp. 457-
178 463, 1994.
- 179 [12] H. M. Ali and A. Ali, "Measurements and semi-empirical correlation for condensate retention
180 on horizontal integral-fin tubes: Effect of vapour velocity," *Applied Thermal Engineering*, vol.
181 71, pp. 24-33, 2014.
- 182 [13] S. Sukhatme, B. Jagadish, and P. Prabhakaran, "Film condensation of R-11 vapor on single
183 horizontal enhanced condenser tubes," *Journal of Heat Transfer*, vol. 112, pp. 229-234, 1990.
- 184 [14] R. Kumar, H. Varma, B. Mohanty, and K. Agrawal, "Augmentation of heat transfer during
185 filmwise condensation of steam and R-134a over single horizontal finned tubes," *International
186 journal of heat and mass transfer*, vol. 45, pp. 201-211, 2002.
- 187 [15] A. Briggs, "Enhanced condensation of R-113 and steam using three-dimensional pin-fin
188 tubes," *Experimental heat transfer*, vol. 16, pp. 61-79, 2003.
- 189 [16] M. Baisar and A. Briggs, "Condensation of steam on pin-fin tubes: effect of circumferential
190 pin thickness and spacing," *Heat Transfer Engineering*, vol. 30, pp. 1017-1023, 2009.
- 191 [17] H. M. Ali and A. Briggs, "Condensation of R-113 on pin-fin tubes: effect of circumferential
192 pin thickness and spacing," *Heat Transfer Engineering*, vol. 33, pp. 205-212, 2012.
- 193 [18] H. M. Ali and A. Briggs, "Condensation heat transfer on pin-fin tubes: effect of thermal
194 conductivity and pin height," *Applied Thermal Engineering*, vol. 60, pp. 465-471, 2013.
- 195 [19] H. M. Ali and A. Briggs, "An investigation of condensate retention on pin-fin tubes," *Applied
196 Thermal Engineering*, vol. 63, pp. 503-510, 2014.
- 197 [20] H. Ali and A. Briggs, "Condensation of ethylene glycol on pin-fin tubes: Effect of
198 circumferential pin spacing and thickness," *Applied Thermal Engineering*, vol. 49, pp. 9-13,
199 2012.
- 200 [21] H. M. Ali and A. Briggs, "Enhanced condensation of ethylene glycol on single pin-fin tubes:
201 effect of pin geometry," *Journal of heat transfer*, vol. 134, p. 011503, 2012.
- 202 [22] H. M. Ali, "Condensation Heat Transfer on Geometrically Enhanced Horizontal Tube: A
203 Review," in *Heat Exchangers-Advanced Features and Applications*, ed: InTech, 2017.
- 204 [23] H. M. Ali and M. Abubaker, "Effect of vapour velocity on condensate retention on horizontal
205 pin-fin tubes," *Energy Conversion and Management*, vol. 86, pp. 1001-1009, 2014.
- 206 [24] H. M. Ali and M. Abubaker, "Effect of circumferential pin thickness on condensate retention
207 as a function of vapor velocity on horizontal pin-fin tubes," *Applied Thermal Engineering*, vol.
208 91, pp. 245-251, 2015.
- 209 [25] H. M. Ali, H. Ali, M. Ali, S. Imran, M. S. Kamran, and F. Farukh, "Effect of Condensate Flow
210 Rate on Retention Angle on Horizontal Low-Finned Tubes," 2016.
- 211
- 212
- 213